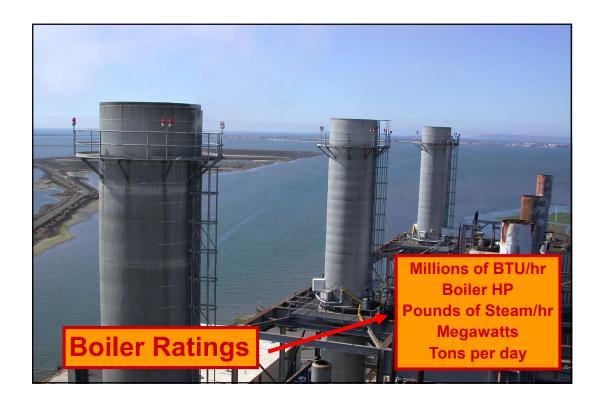
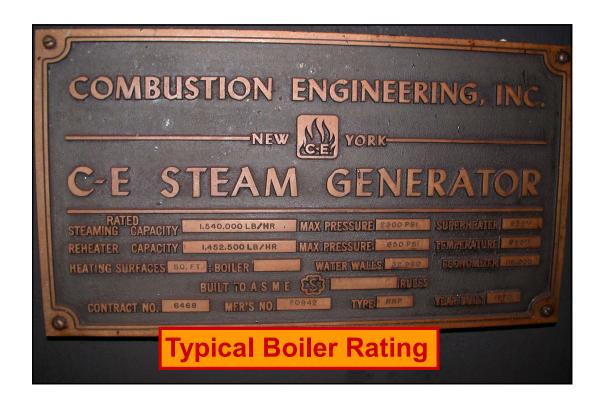


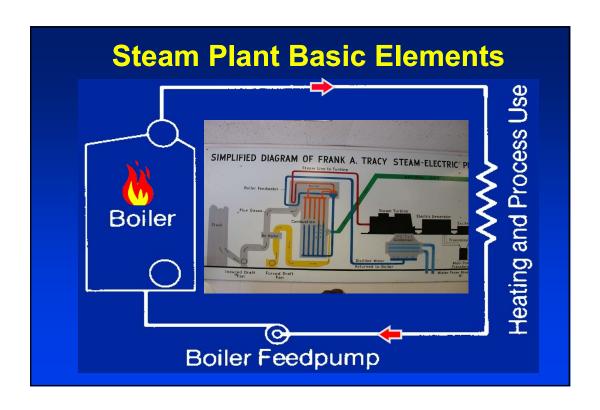


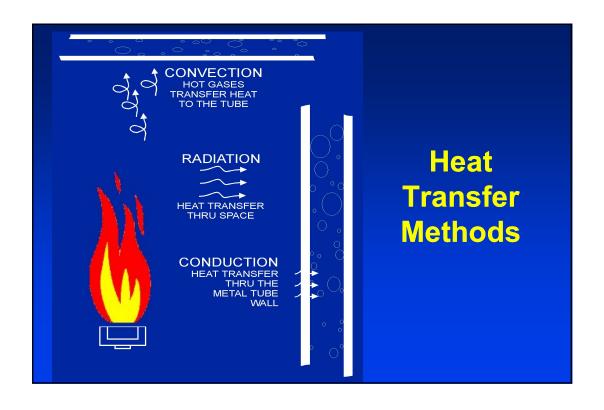
Hot Numbers • British Thermal Unit (BTU) • 1 BTU the amount of energy needed to heat one pound of water one degree Fahrenheit or ≈ energy given off by burning one wooden match • Lower Heating Value (LHV) • Heating value of a fuel not counting heat needed to vaporize water • Higher Heating Value (HHV) • Heating value of a fuel including heat needed to vaporize water



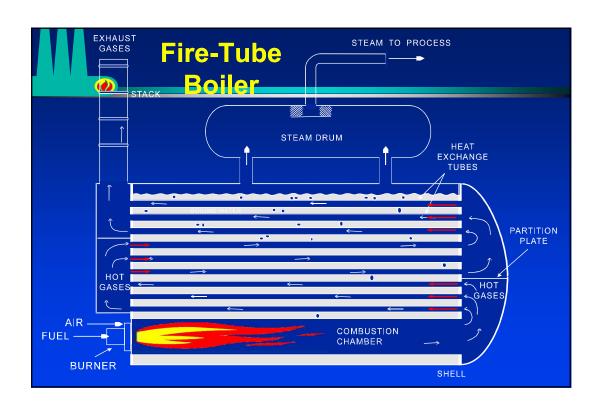




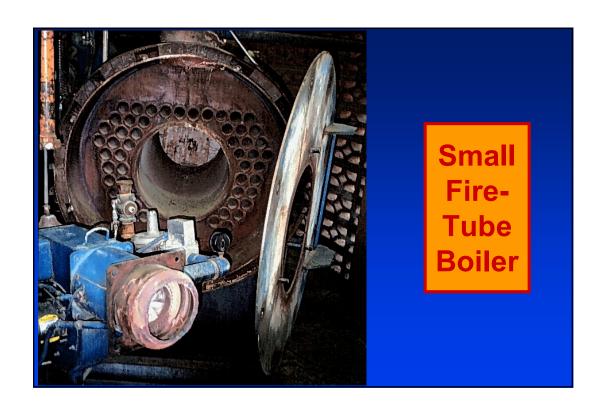




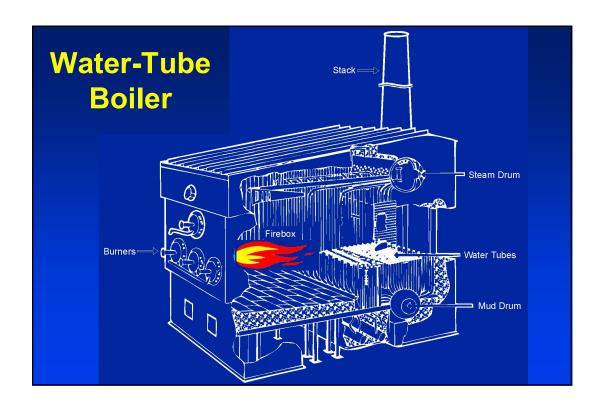


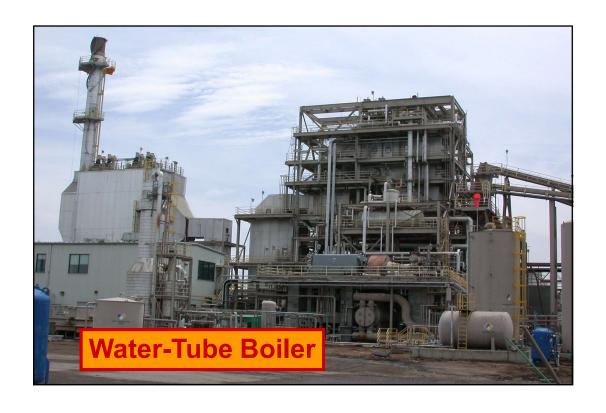


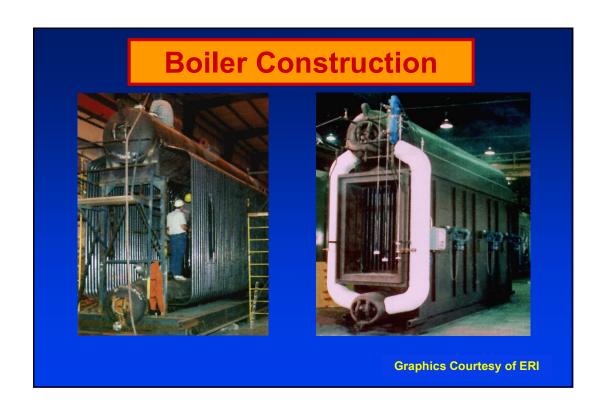




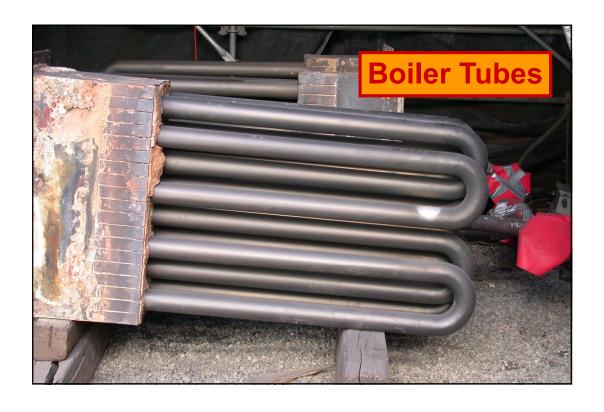


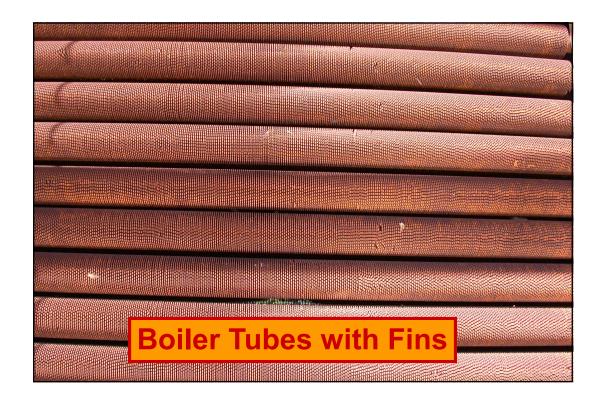


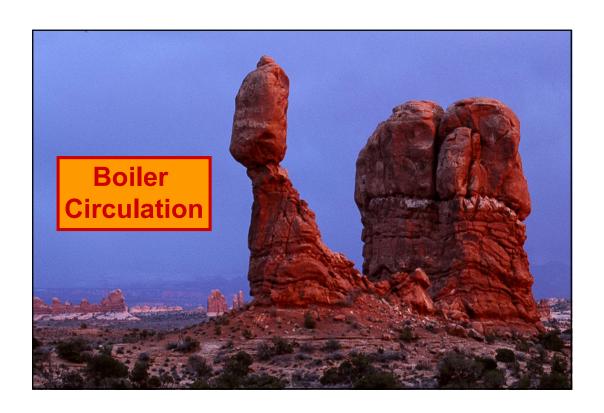


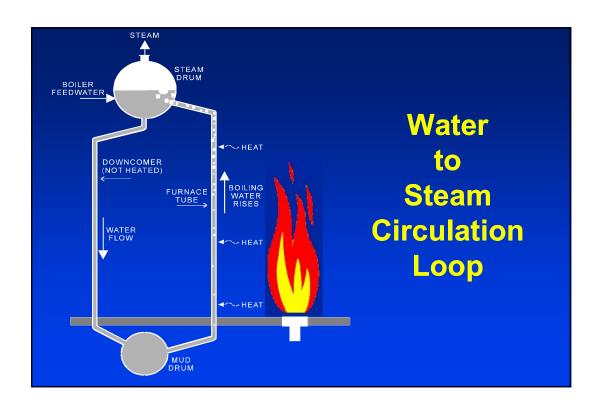


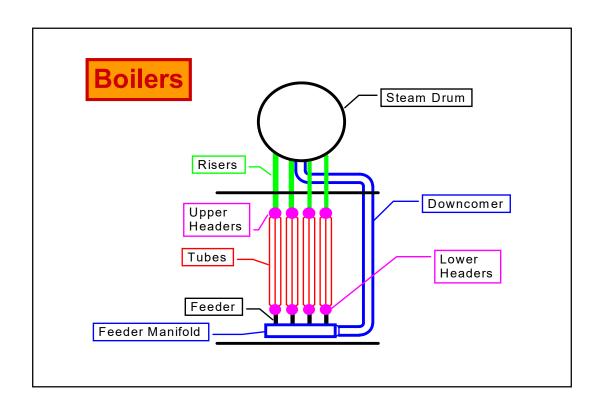


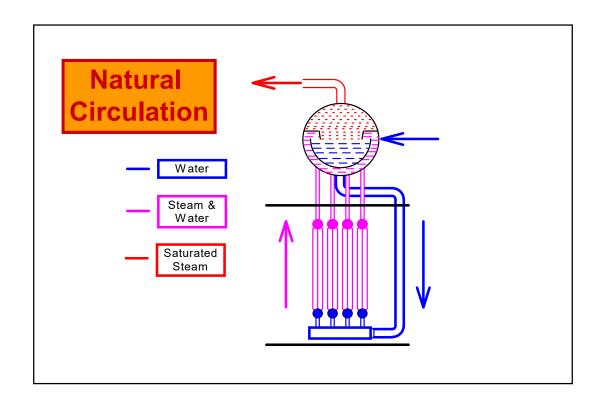


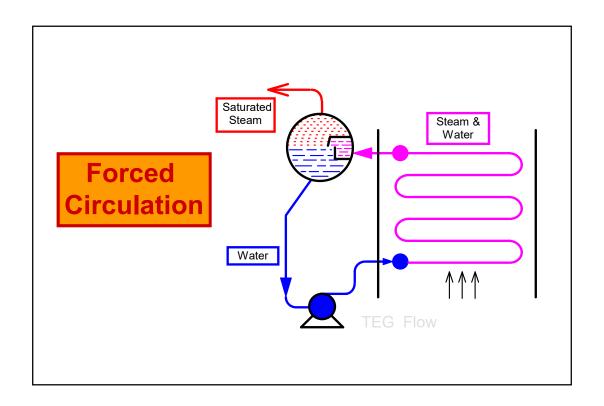












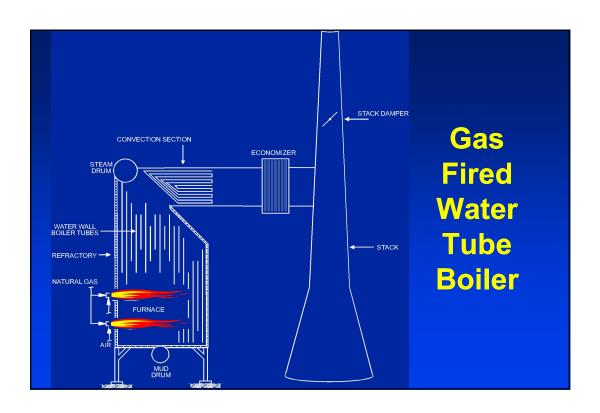


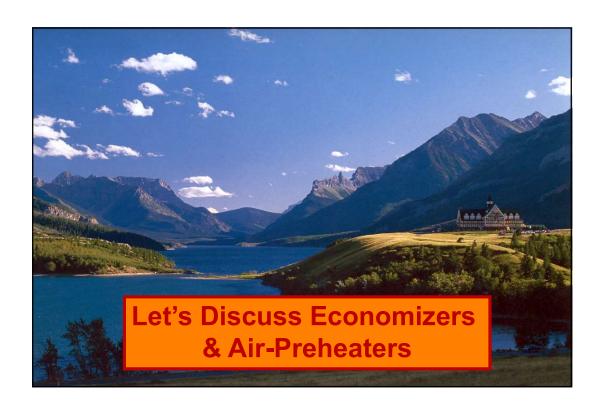




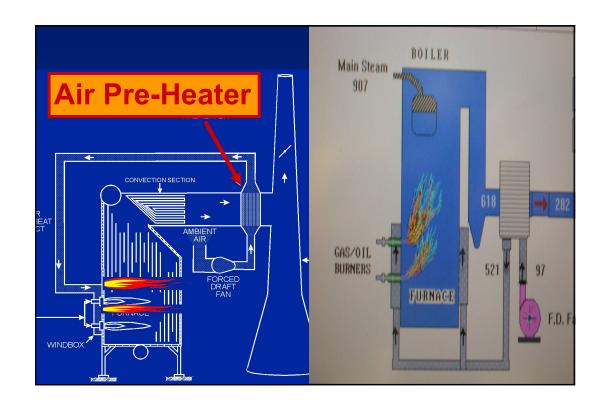






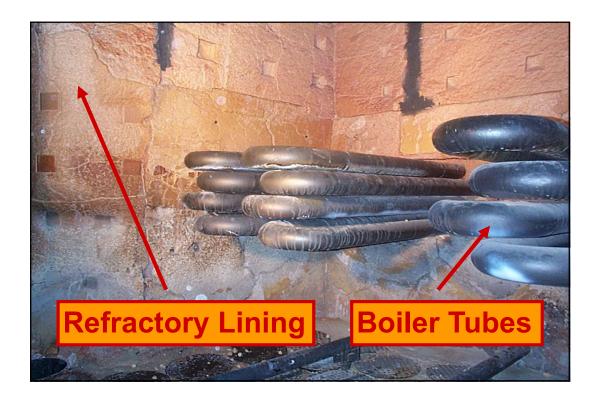


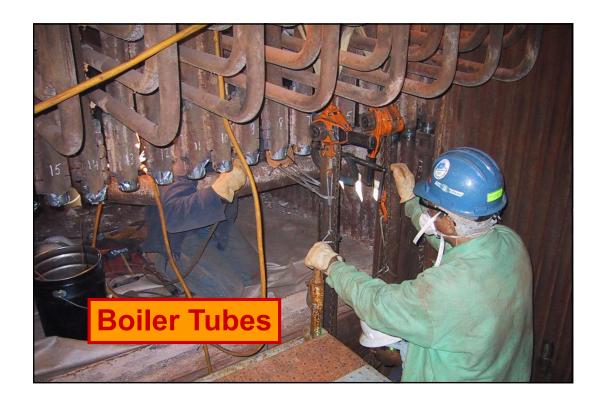


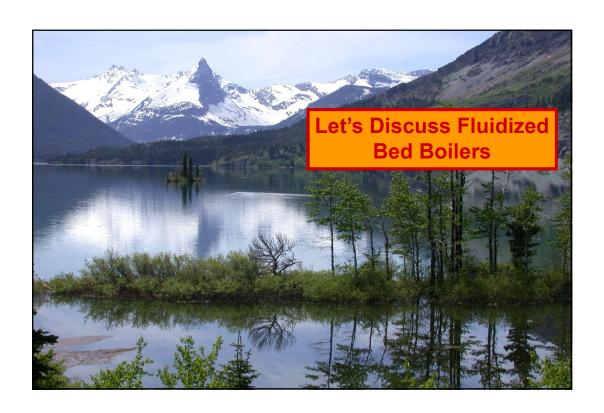


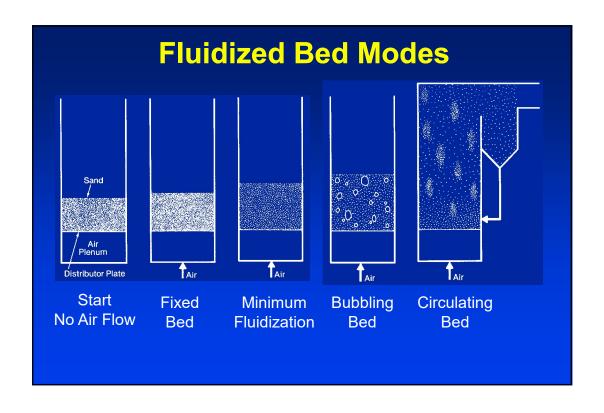


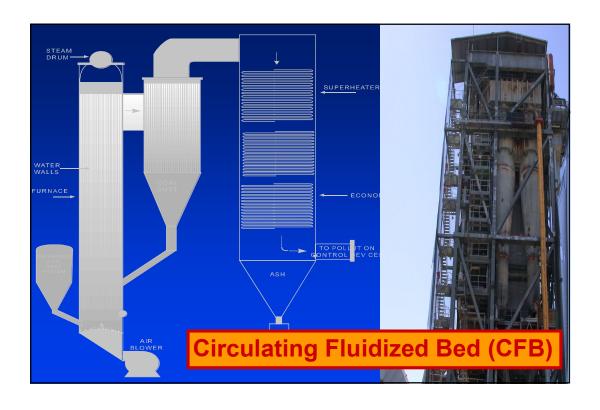


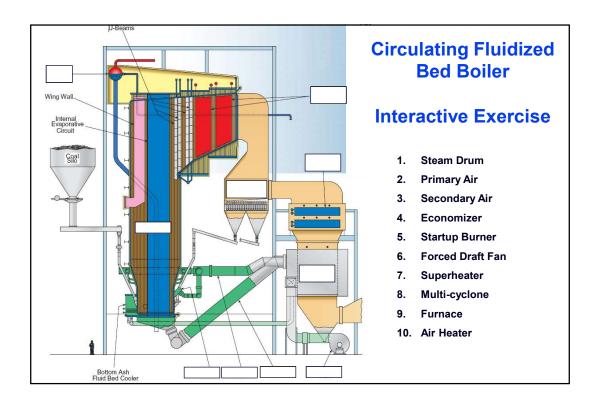


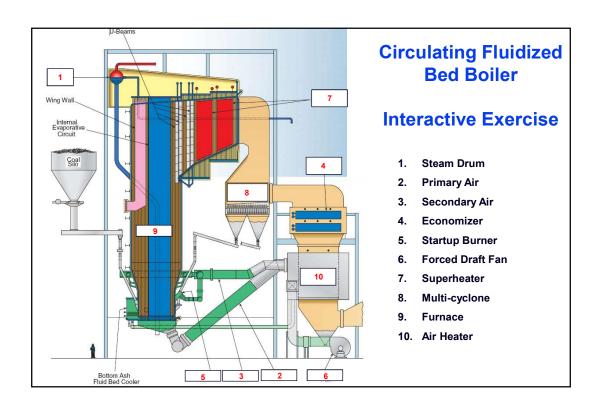


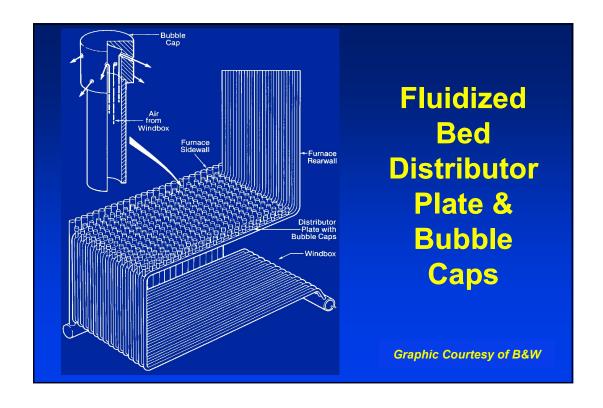




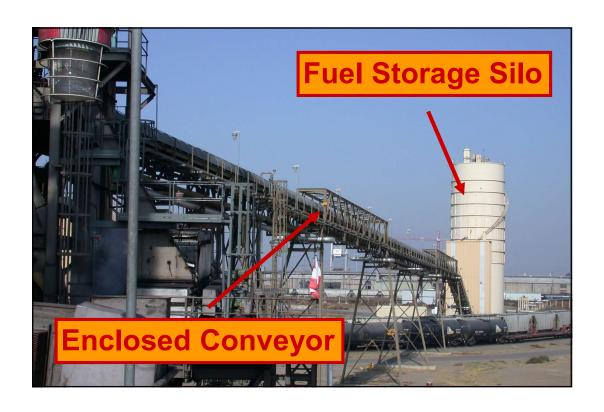


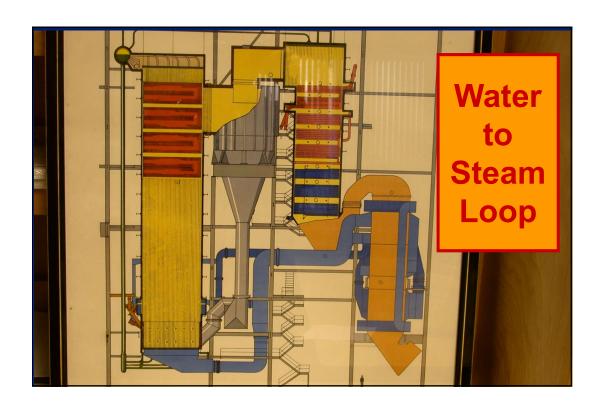


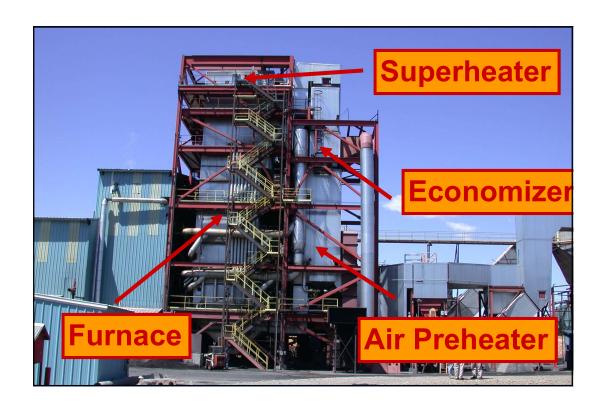


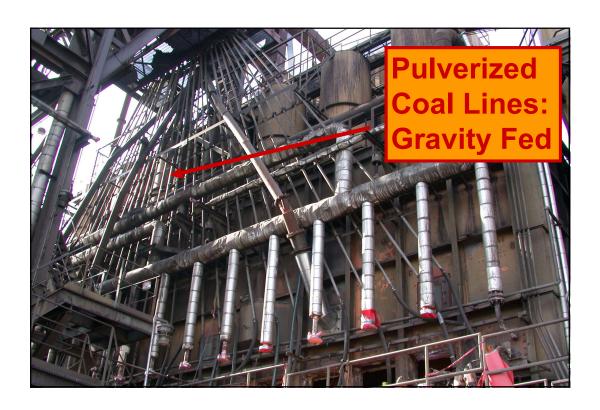


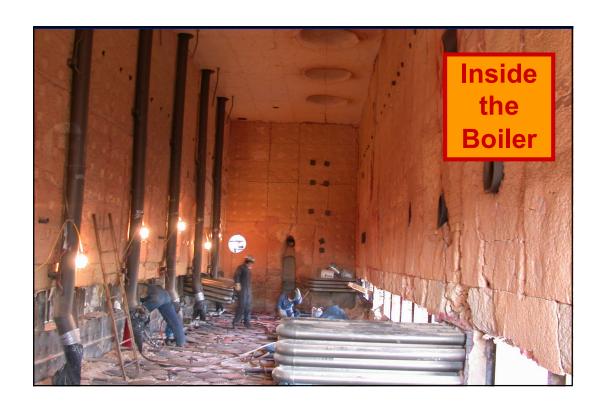


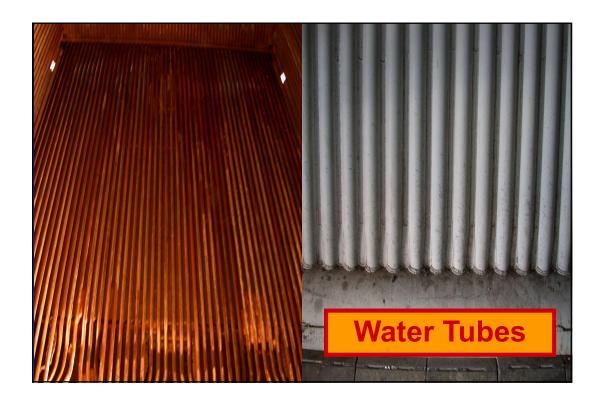




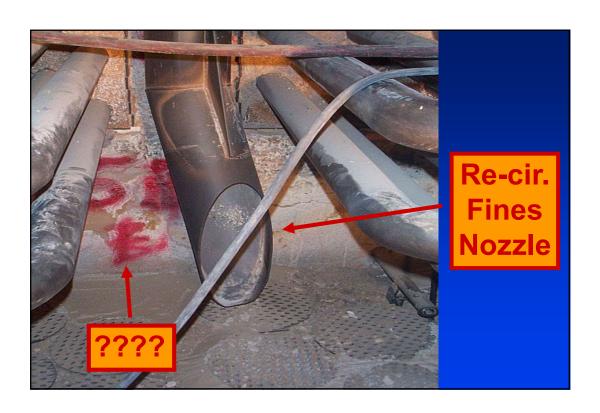


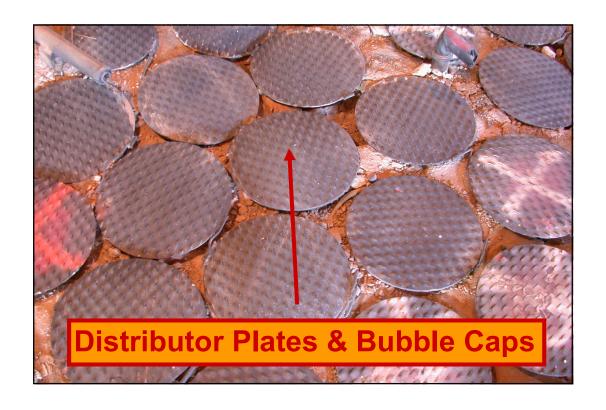






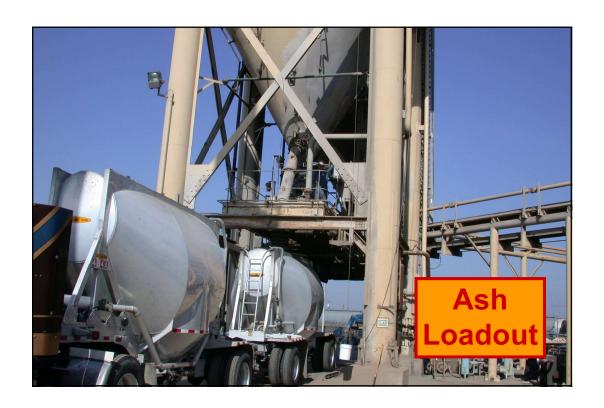


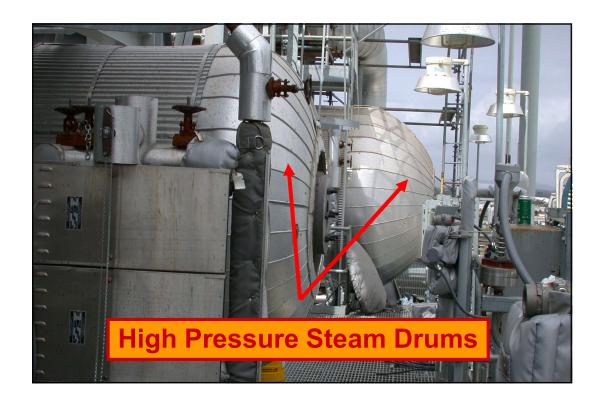




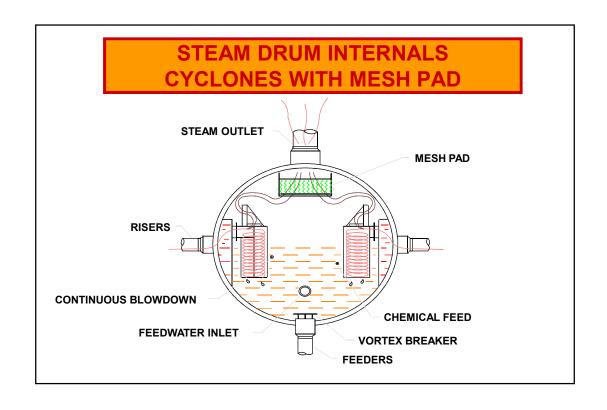


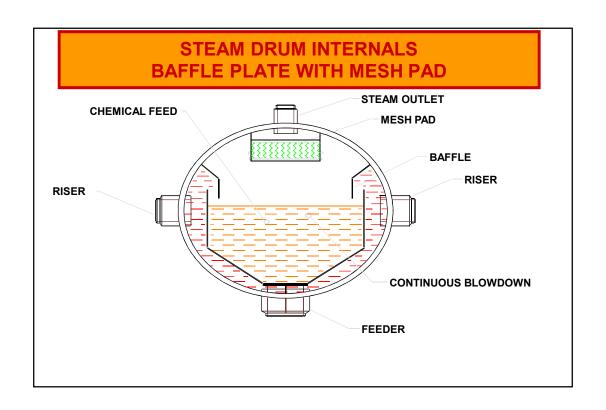


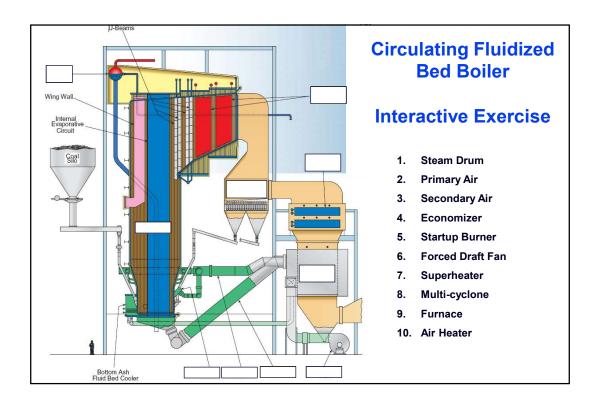


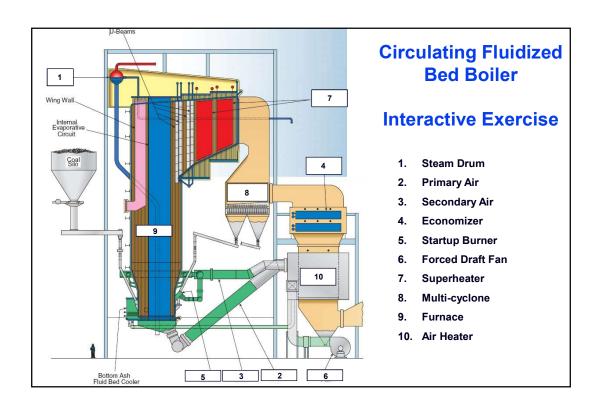


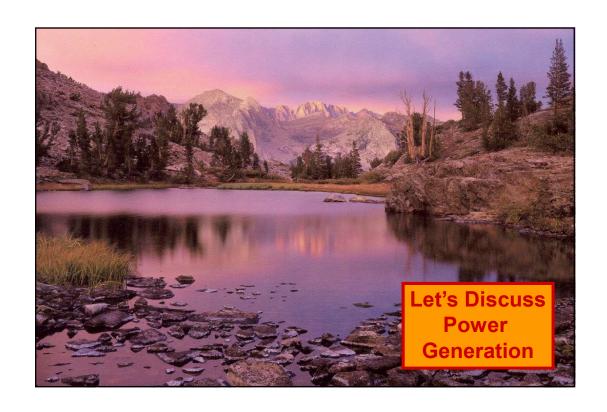










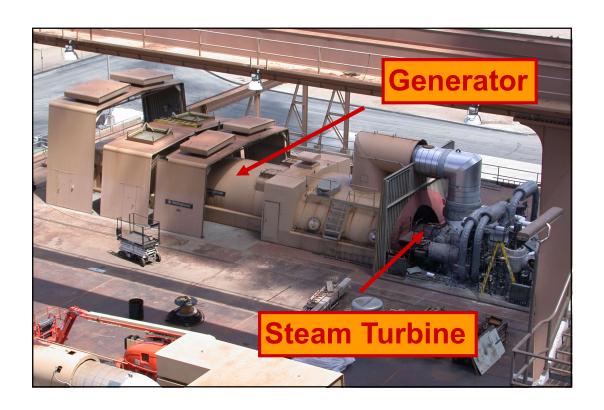








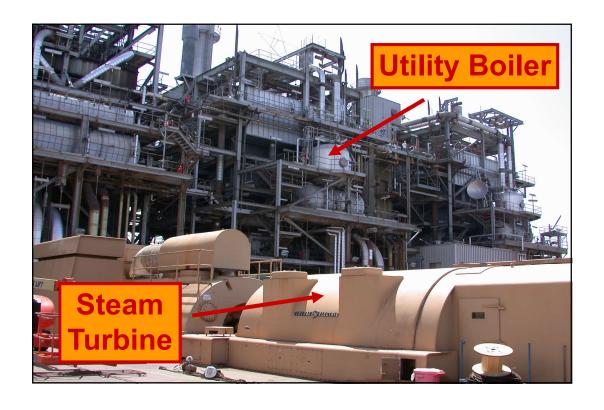






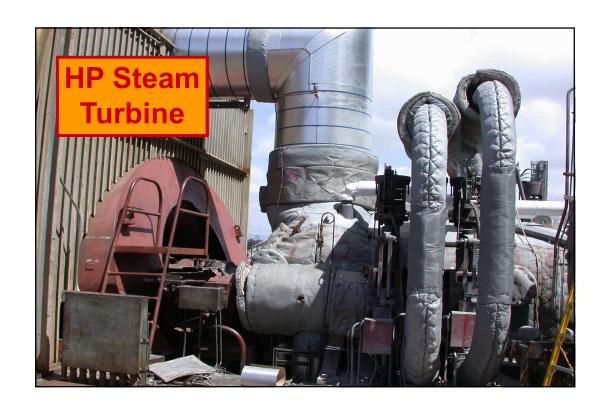


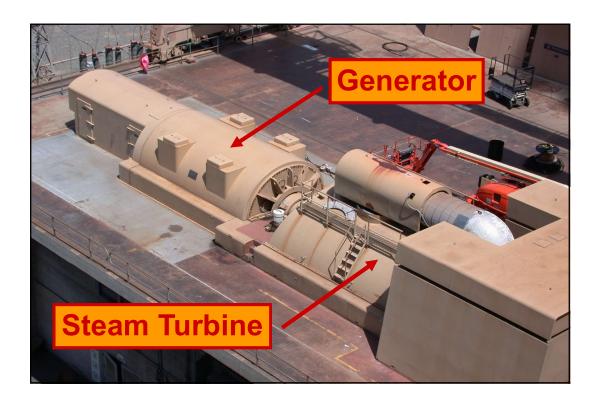








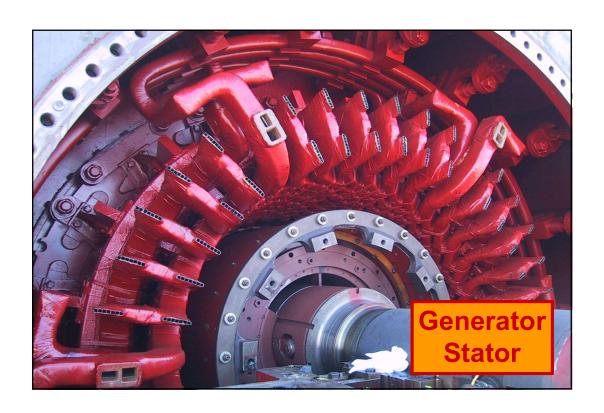




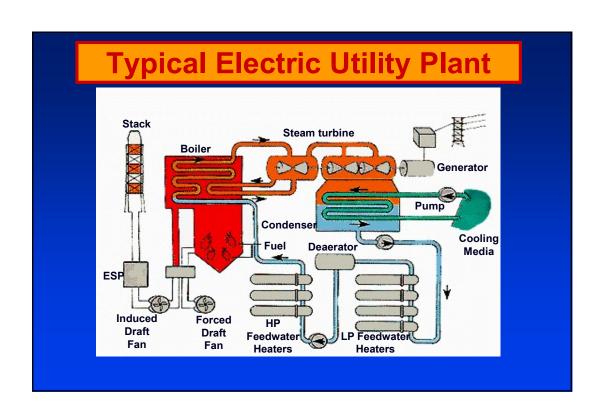




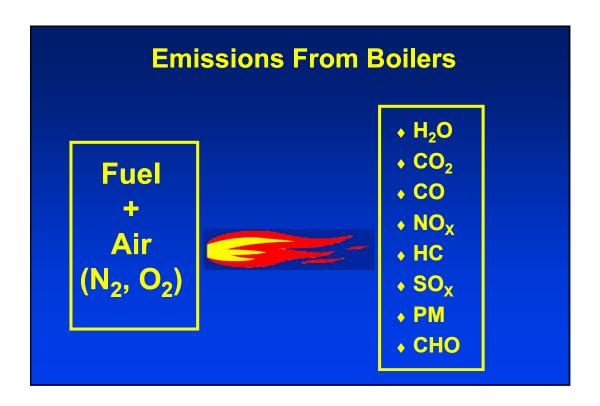












Emissions Control Methods

- Boiler design
- Proper maintenance
- Operating conditions
- Fuel types
- Combustion modifications
- Exhaust treatment



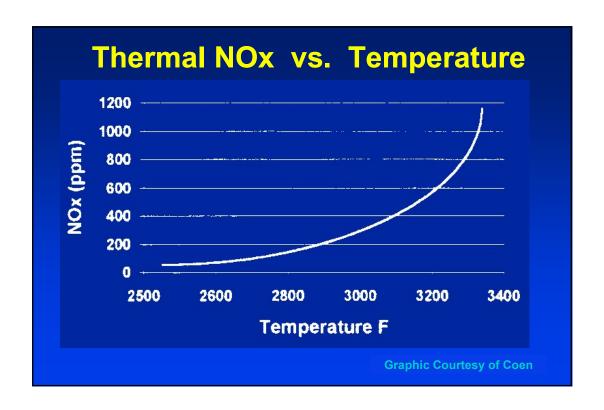
Control of Gaseous Emissions

- Low-NOx burners
- OFA
- Ammonia injection (SNCR)
- Catalysts (SCR)
- FGR
- FGD



Combustion Considerations Time Temperature Turbulence Oxygen Nitrogen





```
COMBUSTION MODIFICATION

    NOx FORMATION

     N + O
     N + OH
                           NO + H

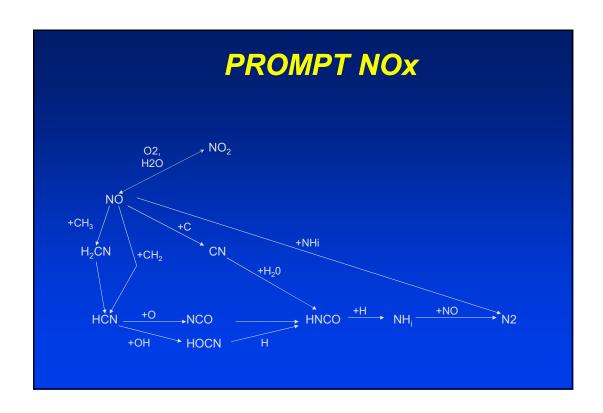
    NOx REDUCTION

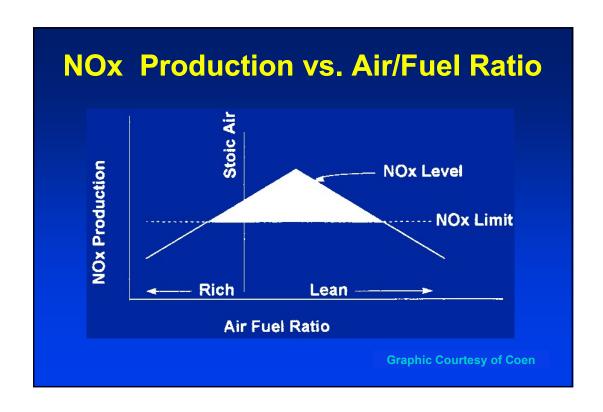
     CH + NO , HCN + O<sub>2 (Reversible)</sub>
                           HCN + OH (Reversible)
     CH<sub>2</sub> + NO
                           CN + O_2
     C + NO
     NH; + NO
                         \sqrt{N_2 + H_2O}
   THESE NOX REDUCTANTS ARE FORMED BY PARTIAL COMBUSTION IN A
     REDUCING ATMOSPHERE
   THE INTERMEDIATE SPECIES, HCN & CN, ARE CONVERTED TO N2, CO2 & H2O IN THE FINAL BURNOUT ZONE
```

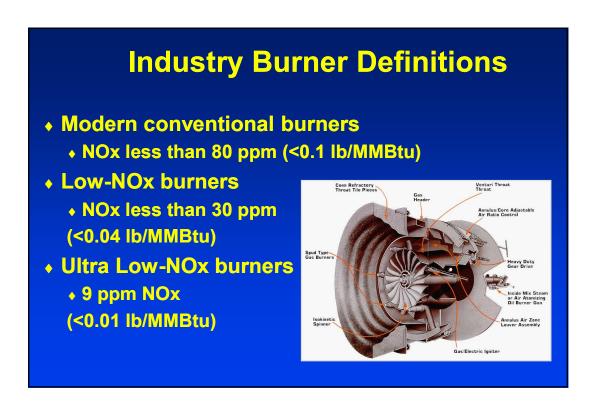
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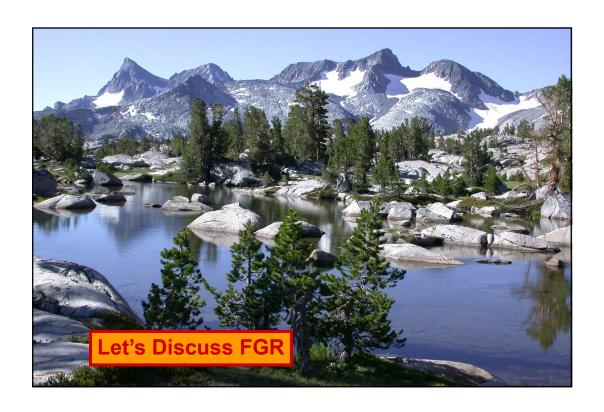
PROMPT NOX

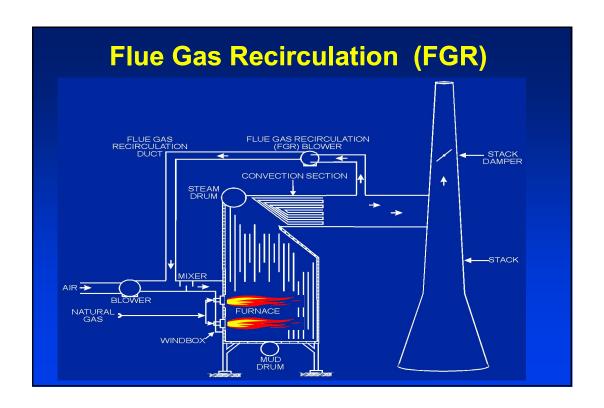
- Rapid Formation <1ms.
- Little affect from temperature.
- Presence of CHi & HCN during initial combustion can contribute to prompt NOx formation in an oxidizing environment, but will inhibit NOx formation in a reducing environment.
- Presence of C & NHi in initial combustion process reduces the formation of prompt NOx.
- Reactor combustion is controlled to a stoichiometry <.6 and a temperature <2400F.

















FGR BURNERS

FEATURES

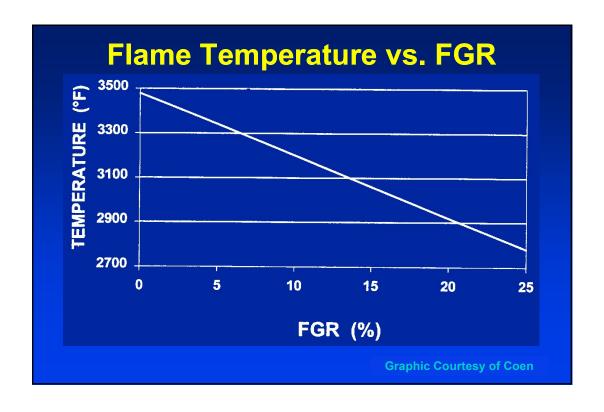
- CAN USE FGR FLOWS AS HIGH AS 40% OF THE TOTAL STACK EFFLUENT
- SOME SYSTEMS OPERATE VERY CLOSE TO THE LIMITS OF FLAMABILITY
- SOME SYSTEMS OPERATE WITH VERY RAPID MIXING, VERY CLOSE TO STOICHIOMETERY.

CON'S

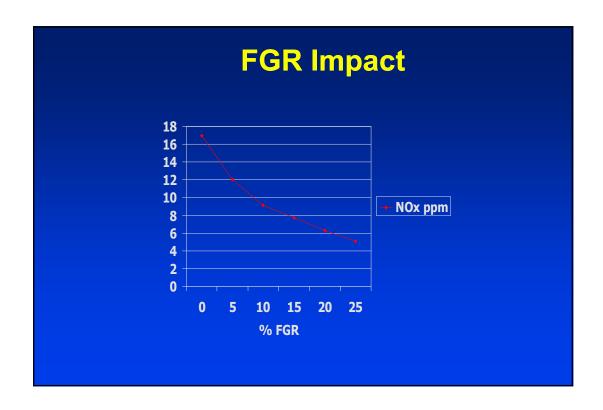
- HIGH ELECTRICAL USAGE (FGR fan HP doubled compared to RX system)
- LOW TEMPERATURE, TRANSLUCENT, FLAME REDUCES HEAT TRANSFER & EFFICIENCY.
- **COMBUSTION INSTABILITY**
- CAN'T CHANGE FIRING RATE FAST ENOUGH TO FOLLOW CHANGING LOAD DEMANDS

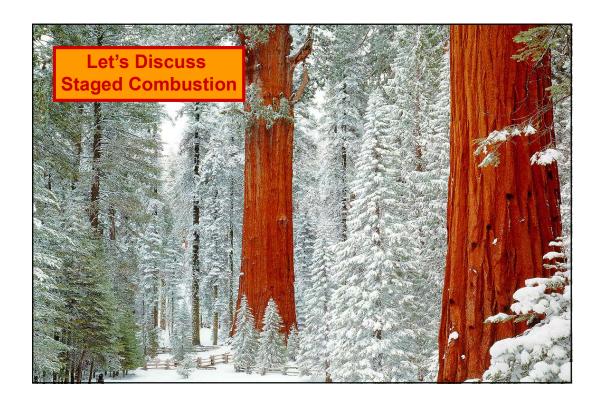
Lower Cost to Industry

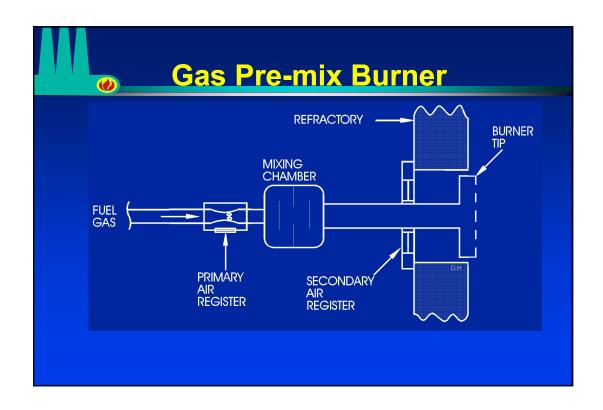
- Simple durable refractory and steel construction results in:
 - Lower initial cost
 - Lower maintenance costs
- ♦ Lower operating cost
 - Less stack losses due to low excess air and low FGR requirements
 - Lower fan costs
 - Eliminates the need for chemicals & catalysts

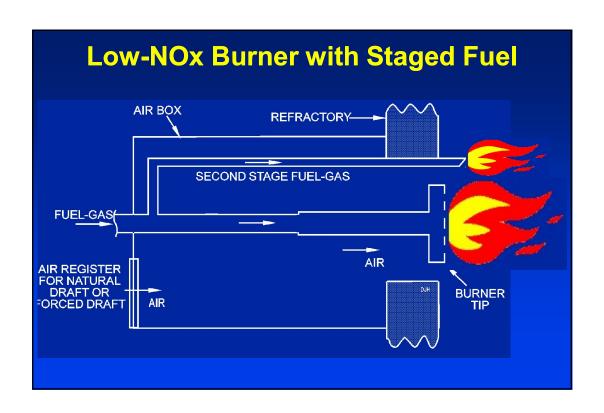


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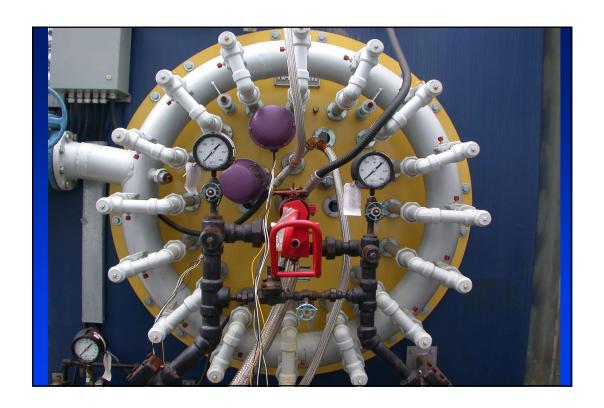


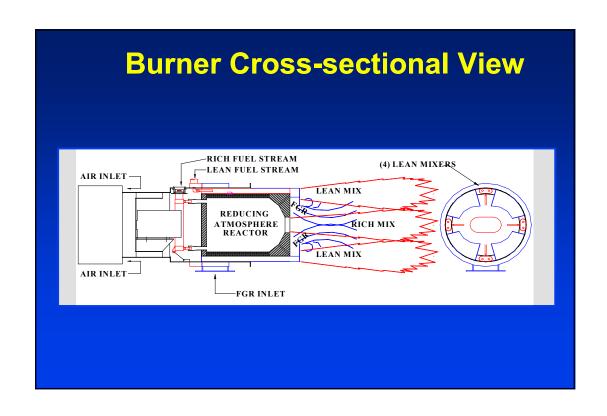


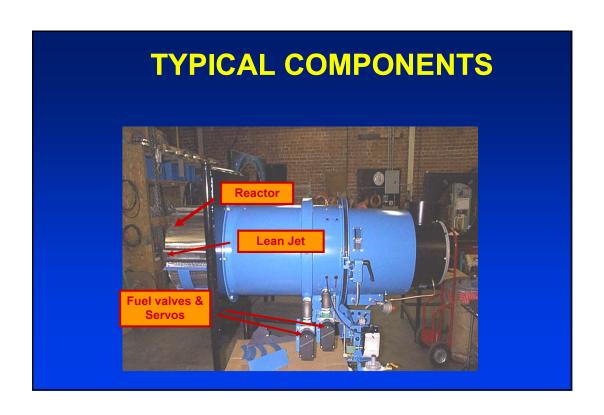




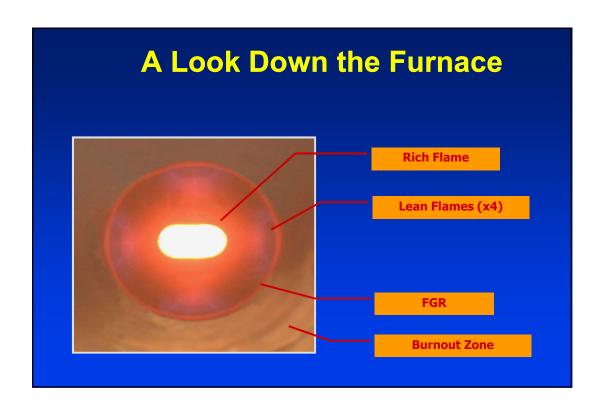


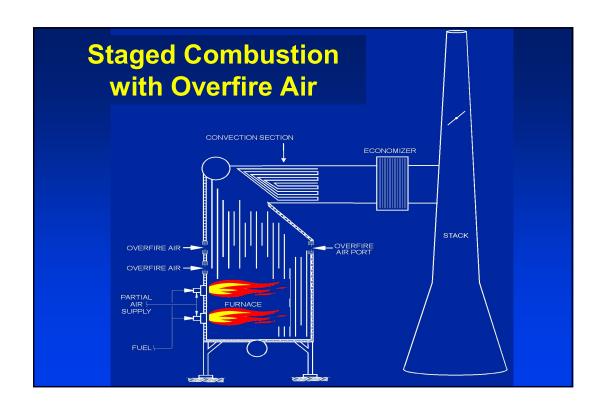




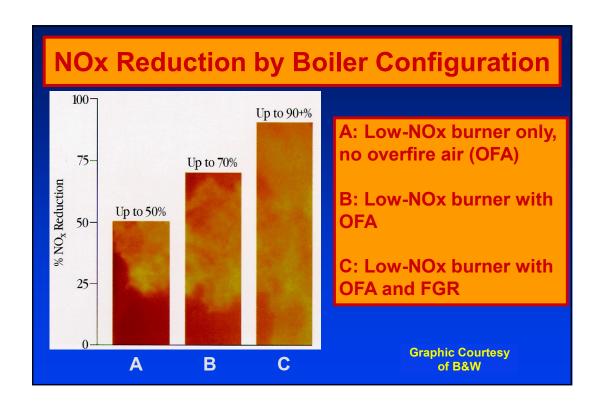


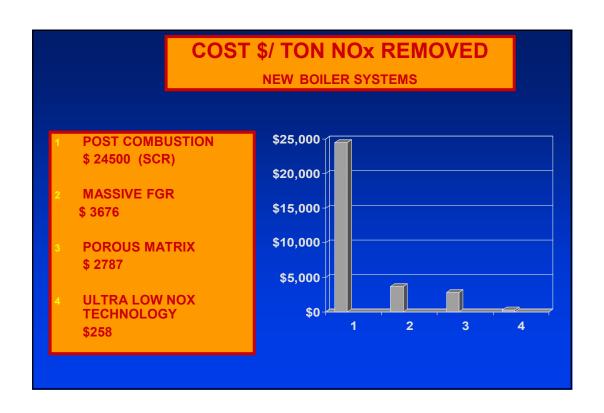












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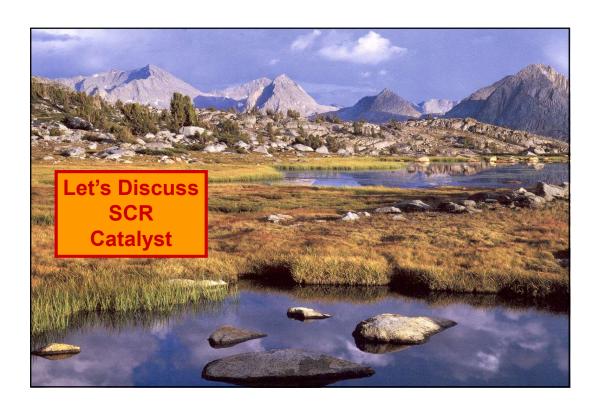
Existing Emissions & Goals

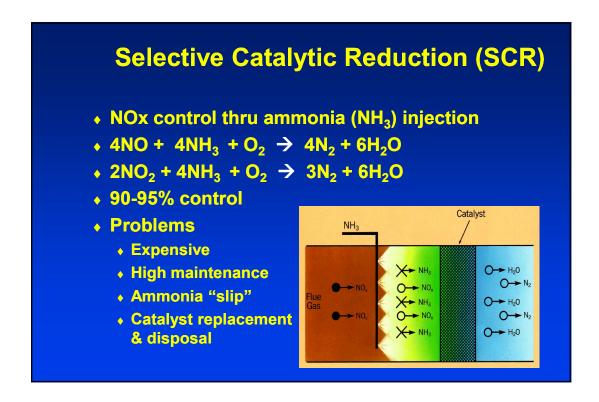
Emission	Existing	Proposed
NOx ppm@3% O2	25.3	5 - 6
CO ppm@ 3% O2	70.2	<50
Stack O2, %	6.2	2.5 – 3.2

Reduce NOx by 75%

Reduce O2 by 48 - 60%

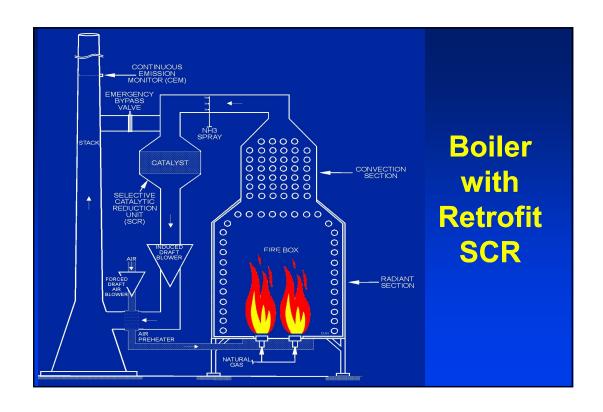
Reducing O2 from 6% to 3% saves this customer 273 CFH of nat gas







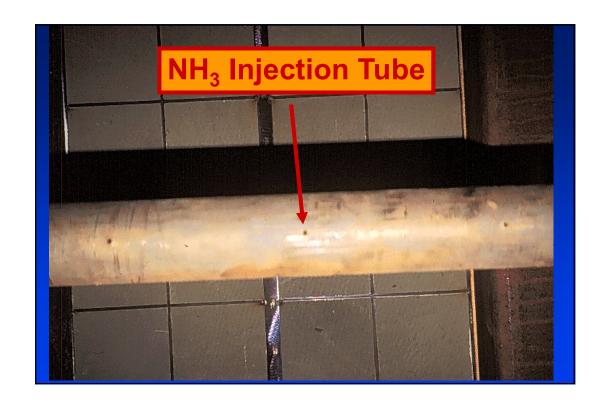
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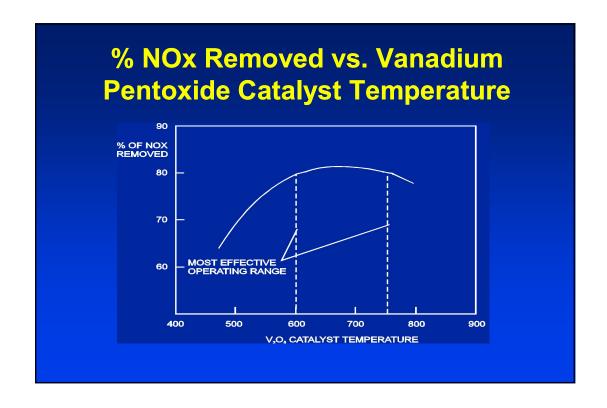




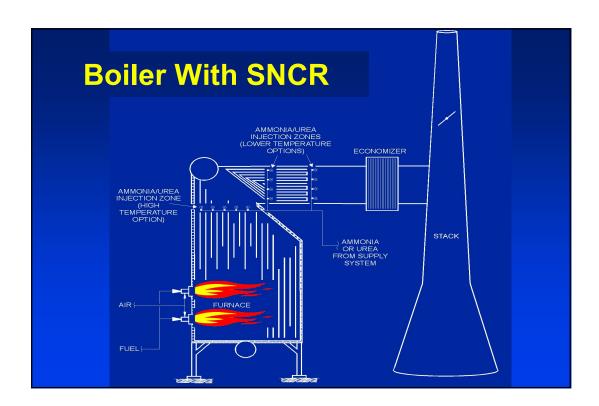












Selective Non-Catalytic Reduction

- NOx control through ammonia or urea injection
- No catalyst necessary
- Temperature range 1400 °F 1700 °F
- Injected upstream of convection section

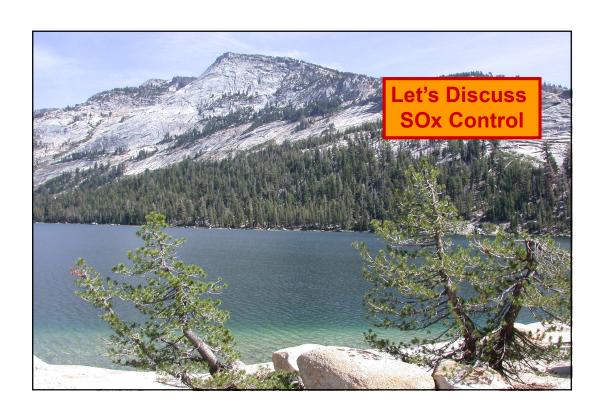
70

- 80% control under normal conditions
- Problems:
 - Changing flue temperatures with changing load
 - Formation of ammonium salts
 - Ammonia slip



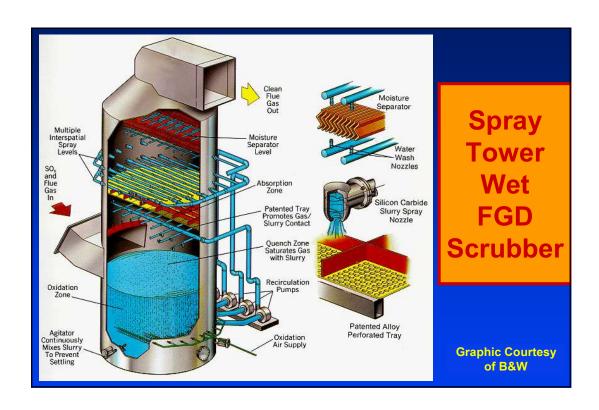
October 2020

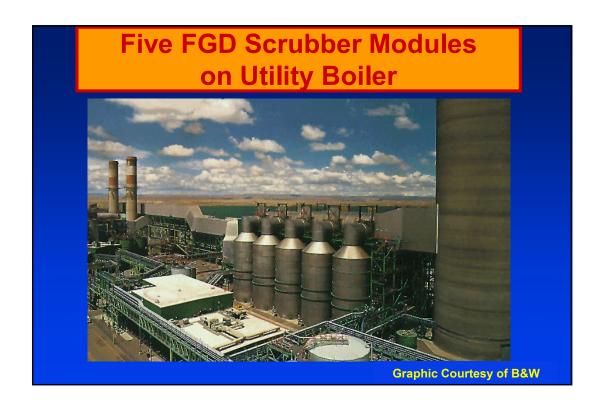
Comparison of NOx Reduction Technologies					
Technology	Approx. Reduction	Approx. lbs/MMBTU	Approx. ppmv @ 3% O2		
Standard burners	Base case	0.14	120		
Low NOx burners	60%	0.06	45		
Ultra Low NOx burners – I st gen.	80%	0.03	25 - 30		
Ultra Low NOx burners – 2 nd gen.	95%	0.007	6 - 9		
FGR	55%	0.025	20		
Compu- NOx w/ FGR	90%	0.015	15 - 20		
SNCR	80%	0.033 - 0.085	27 - 70		
Catalytic Scrubbing	70%	0.017 - 0.044	14 - 36		
SCR	90 – 95%	0.006 - 0.015	5 - 12		

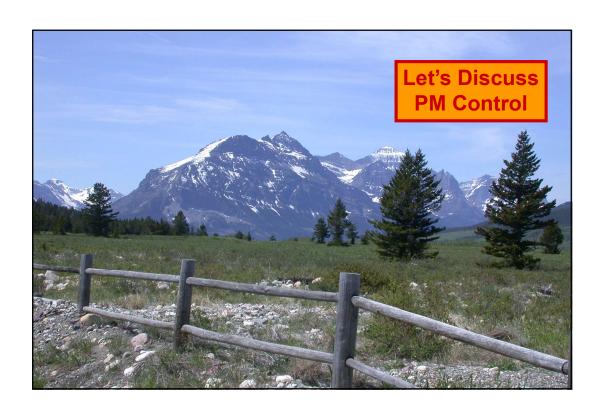


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Sulfur Content of Various Fuels		
Fuel	Sulfur Percent by Weight	
Natural gas	0.0005	
LPG	0.001	Fuel
Fuel Oil No. 1	0.01 to 0.3	
Fuel Oil No. 2	0.05 to 0.5	Sulfur
Diesel Motor Fuel	0.0015	
Fuel Oil No. 4	0.2 to 1.75	Content
Fuel Oil No. 5	0.5 to 1.75	
Fuel Oil No. 6	0.5 to 1.75	
Low Sulfur Fuel Oil No. 6	0.5	
Subbituminous coal from Rocky Mt. states	0.3 to 1	
Petroleum coke	2 to 10	

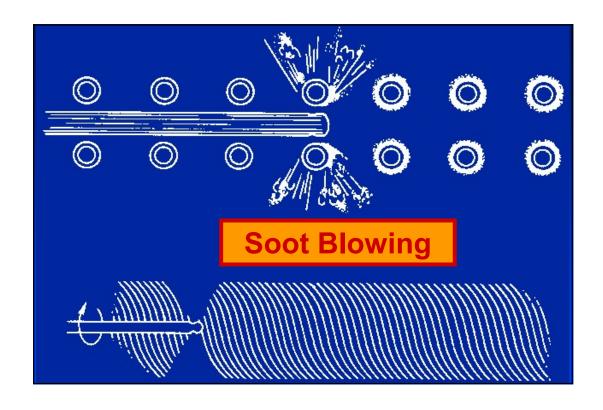






Control of Particulate Emissions Settling chambers Cyclones Baghouses ESPs Scrubbers

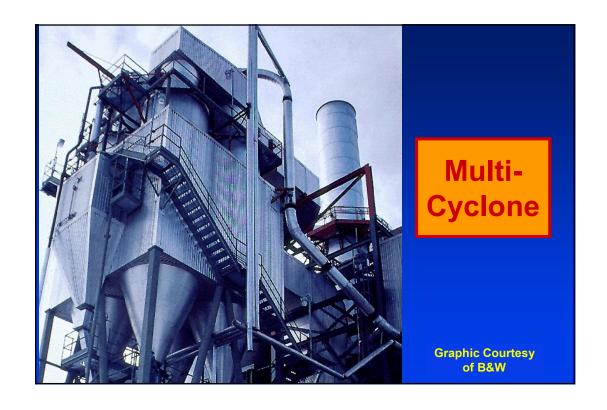


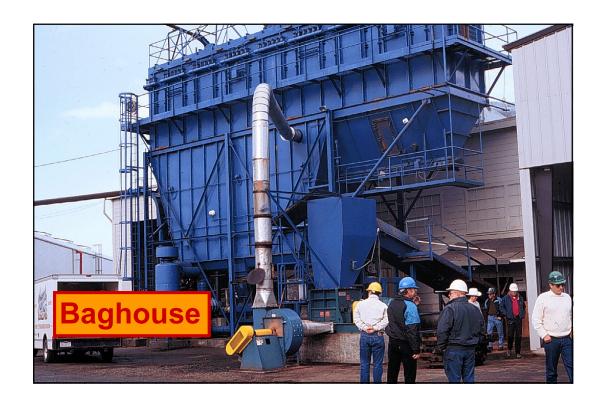










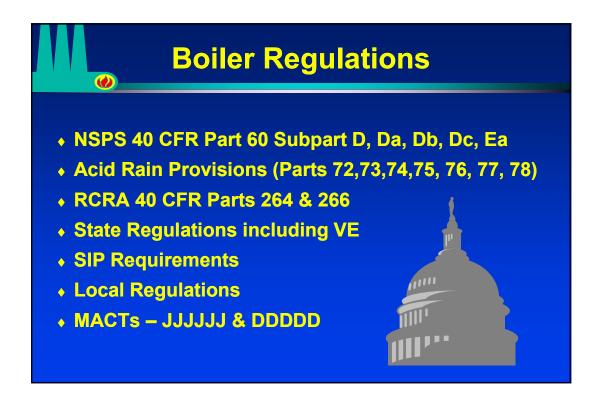








Regulatory Requirements Federal, state, and local requirements Boiler specific limits Permit requirements Monitoring requirements Visible emission limits Nuisance regulations Breakdowns & variances



Boiler Emission Limits NOx, SO2, particulate, and opacity values for boilers are based on applicable subpart, heat input, date built or modified, and fuel used States and districts may have more stringent limits

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BACT in CA		
Type of Control	NOx Limits	
Natural Gas Fired with SCR or equal	6 - 9 ppmvd @3% O ₂ (0.011 lb/MMBTU	
Natural Gas Fired with Ultra Low NOx Burner	15 ppmvd @3% O ₂ (0.018 lb/MMBTU	
Natural Gas Fired with Low NOx Burner	20 ppmvd @3% O ₂ (0.024 lb/MMBTU	

BARCT & RACT		
Type of Control	NOx Limits	
Natural Gas Fired with Low NOx Burner	9 - 30 ppmvd @3% O ₂ 0.036 lb/MMBTU	
Natural Gas Fired Units (< 40 MMBTU/hr)	74 ppmvd @3% О ₂ 0.085 lb/ммвти	
Solid Fuel Fired Boilers	0.20 Ib/MMBTU	
Municipal Solid Waste	200 ppmv @12% CO ₂ 0.24 lb/MMBTU	

Permit Categories

- 1. Emissions Limitations
- 2. Equipment Requirements
- 3. Operating Conditions
- 4. Monitoring and Recording Requirements
- 5. Compliance Testing
- 6. General Requirements



Testing and Monitoring

- Continuous Monitoring System
- Stack Testing
- Process Monitors
- Recordkeeping

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Continuous Monitoring Types

- Opacity Transmissometers
- + NO_X
- SO₂
- + CO
- O₂ and/or CO₂
- Ammonia
- Mercury Semi-Continuous

Source Testing

- Particulate Matter (PM, PM10, PM2.5)
- NOx, SO2, CO, Ammonia
- Mercury and Other Metals
- Hydrogen Chloride
- Formaldehyde
- Visible Emissions (Method 9)

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Control Device Parameters

- ESP Spark Rate and Fields in service
- Baghouse Pressure Drop
- Scrubber Pressure Drop and Liquor Flow Rate
- Fuel Usage

Alternative Monitoring

- Portable analyzer monitoring of NOx, CO, O₂
- Determination of FGR rate
- Burner mechanical adjustments
- O₂ Trim concentration
- FGR valve(s) setting

Portable Combustion

Analyzer





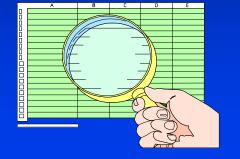




Reasons for Inspections Compliance determination Complaint investigation Source plan approval Review or renewal of permits Special studies

Inspection

- Visible emission evaluation
- General upkeep & maintenance
- Monitoring instruments & records
- Fuel type and quality
- Maintenance records
- Operational records
- Source tests





Inspector Safety

- Proper equipment
- Plant warnings
- Heat
- High pressure steam



- Noise
- Moving parts
- Inhalation hazards
- Hazardous materials
- Machine disintegration
- Fires
- Other hazards & traps





















