

# APTI Course 427

## Combustion Source Evaluation

### Chapter 5: Air Pollution Formation

# Chapter Overview (outline)

- Introduction
- Acid Gases
- Particulate Matter
- Metals
- Nitrogen Oxides
- Smoke, Carbon Monoxide & Organic Compounds
- Opacity

# Introduction (outline)

- Types of Pollutants
- Actual Emission Rates
- Potential Emission Rates
- Clean Fuels

# Types of Pollutants

- Products of Incomplete Combustion (PIC)
- Pollutants resulting from inorganic contaminants in the fuel
- $\text{No}_x$
- Ozone,  $\text{PM}_{2.5}$

# Actual Emission Rates

- Measurements
- Mass balances
  - Gives an upper limit
- AP-42
  - Generic, not specific

# Potential Emission Rates

**Table 5-1. Emissions Originating in the Fuel**

<i>Fuel Constituent</i>	<i>Fuel Concentration</i>		<i>Pollutant Concentration</i>		<i>Primary Method of Control</i>
	<i>No. 6 Oil</i>	<i>Coal</i>	<i>Species</i>	<i>Conversion</i>	
Sulfur <sup>(1)</sup>	0.5 – 2%	1 – 4%	SO <sub>2</sub>	99%	Low sulfur fuel
			H <sub>2</sub> SO <sub>4</sub>	1%	Very low excess air
Ash	<0.05%	10%	Particulate	20 – 98%	Dust collector
			PM-10, 2.5	20 – 80%	Dust collector
Nitrogen <sup>(2)</sup>	<0.5%	1%	NO <sub>x</sub>	10 – 50%	Combustion mod
Chloride	(low)	(low)	HCl	100%	Fuel specs
C <sub>n</sub> H <sub>m</sub>	98%	85%	C, CO, HC	0 – small	Combustion tuning

Notes: [1] SO<sub>4</sub> in the fuel does not convert to SO<sub>2</sub> or sulfuric acid.  
 [2] Only organic nitrogen contributes to NO<sub>x</sub> formation.

# Potential Emission Rates (cont.)

If 100% of contaminant converts to pollutant – eqn 5-1

$$\frac{\text{lb}}{\text{mmBTU}} = \frac{\% \text{ contaminant}/100}{\text{HHV} \left( \frac{\text{BTU}}{\text{lb}} \right) / 10^6} \times \frac{\text{lb pollutant}}{\text{lb contaminant}}$$

# Example 5-1. Potential emissions

- Determine the potential SO<sub>2</sub> emission rate for 3% sulfur coal with HHV = 12,000 BTU/lb.

$$\frac{0.03 \left( \frac{\text{lb S}}{\text{lb coal}} \right)}{0.012 \left( \frac{\text{mmBTU}}{\text{lb coal}} \right)} \times \frac{64}{32} = 5 \left( \frac{\text{lb of SO}_2}{\text{mmBTU}} \right)$$



# Clean Fuels

- Natural gas
  - Clean burning
  - Benefits catalysts
  - Significant pollutants
- Distillate oil
  - Some sulfur content
  - No premixed combustion

# Acid Gases (outline)

- Sulfur Oxides
- Hydrochloric Acid

# Sulfur Oxides

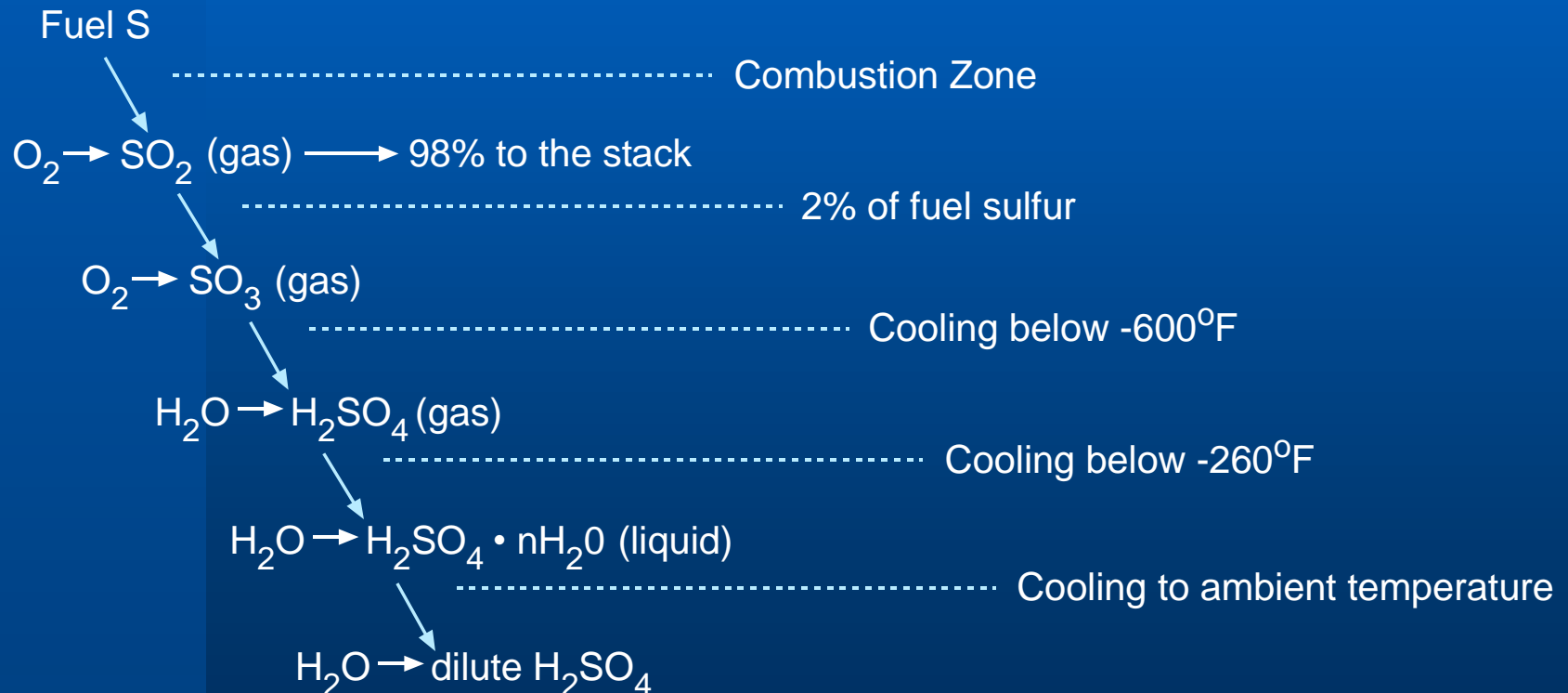
- $\text{SO}_2$ 
  - Emissions control by fuel S limits
  - Oxidizes slowly in the atmosphere

- $\text{SO}_3$  and Sulfuric Acid



# Fuel Sulfur Conversion

## Sulfur Oxidation



## Example 5-2.

If 2% of the sulfur in oil with 1.5% S is converted to  $\text{SO}_3$ , what is the flue gas concentration?

Solution: (a) Determine emission rate (lb/mmBTU)

$$\frac{0.015 \left( \frac{\text{lb S}}{\text{lb oil}} \right)}{0.0185 \left( \frac{\text{mmBTU}}{\text{lb oil}} \right)} \times \frac{80 \left( \frac{\text{lb SO}_3}{\text{lb S}} \right)}{32} \times 2\% = 0.0405 \left( \frac{\text{lb SO}_3}{\text{mmBTU}} \right)$$

# Example 5-2. (cont'd)

Convert this to ppm by volume

$$\frac{0.0405 \left( \frac{\text{lb SO}_3}{\text{mmBTU}} \right)}{10,500 \left( \frac{\text{ft}^3 \text{ fluegas}}{\text{mmBTU}} \right)} \times \frac{385}{80} \left( \frac{\text{ft}^3 \text{ SO}_3}{\text{lb SO}_3} \right) = 18.6 (10^{-6}) = 18.6 \text{ ppm SO}_3$$

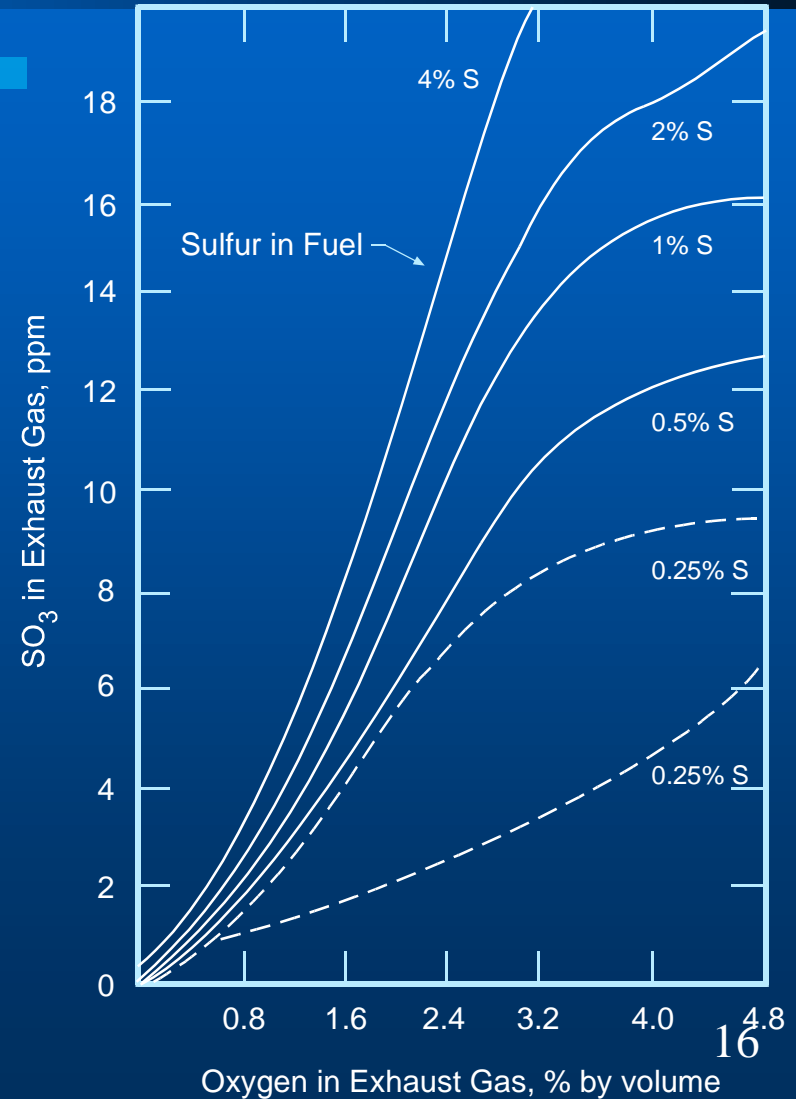
Correct this to a standard dilution level (3% O<sub>2</sub>)

$$18.6 \text{ ppm} \times \frac{20.9\% - 3\%}{20.9\%} = 15.8 \text{ ppm SO}_3 @ 3\% \text{ O}_2$$

# Conversion of Fuel Sulfur to $\text{SO}_3$

- Small but uncertain
- Vanadium influence
- Ash quantity and pH

# Conversion of Fuel Sulfur to $SO_3$ (cont.)

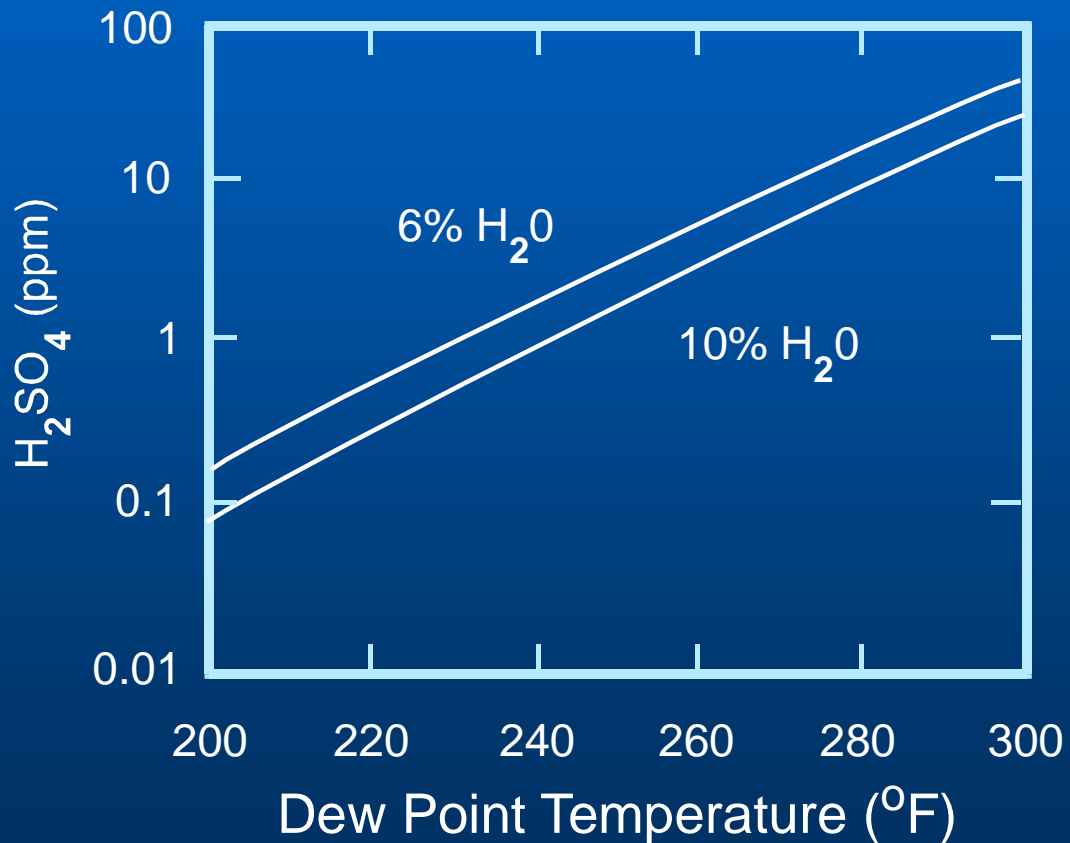




# Sulfuric Acid Effects

- Plume impacts
  - Regional visibility
  - Plume behavior
  - Downwash
- Corrosion
  - Damage
  - Fallout

# Sulfuric Acid Dew Point



# Ash Interaction with Sulfur Oxides

- Coal ash
  - Acid interaction
  - Amount of scrubber solids
- #6 Oil ash
- Additives

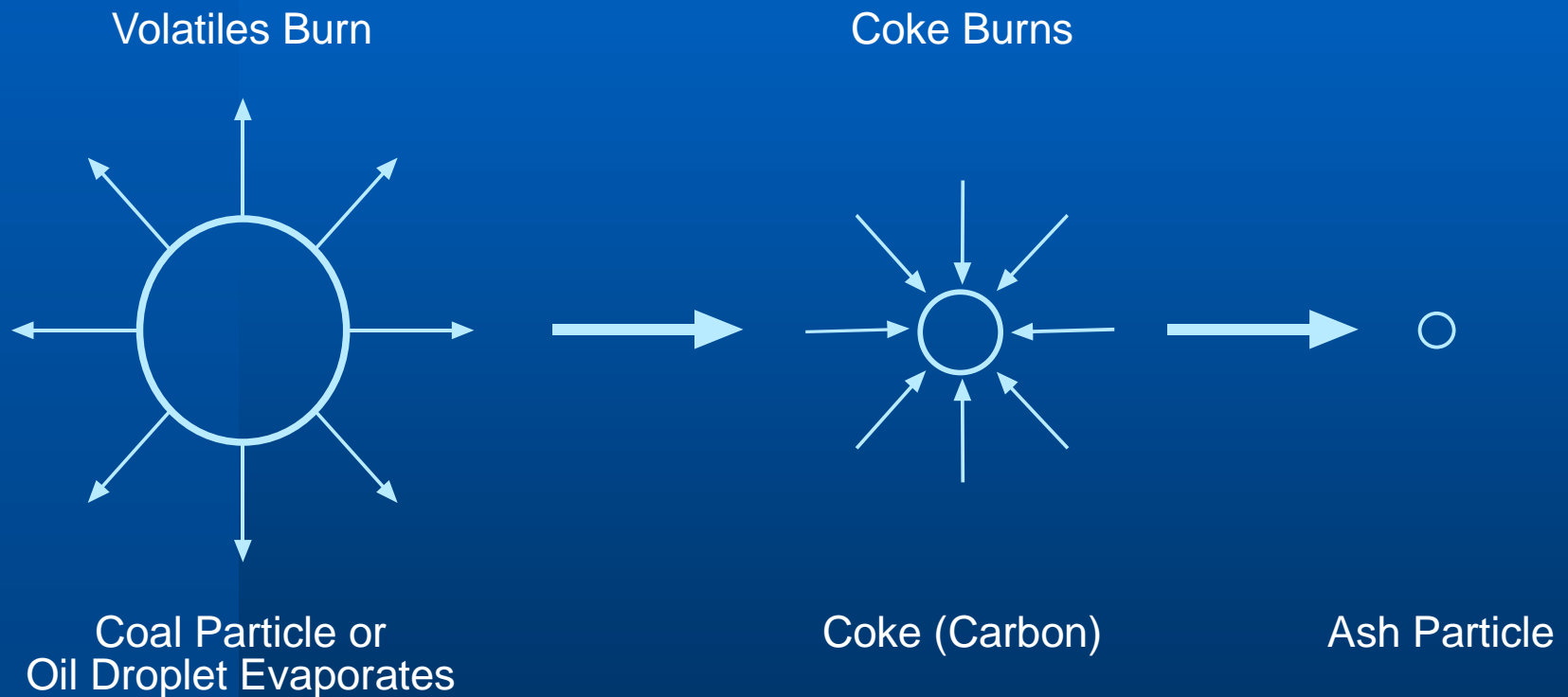
# Hydrochloric Acid

- Organic vs Inorganic conversion  $\text{Cl} \rightarrow \text{HCl}$
- $\text{Cl}_2$  versus  $\text{HCl}$
- Cl contribution to dioxins

# Particulate Matter (outline)

- Particle Formation – two groups
  - Large Particles (mass)
  - Fine Particles (visibility)
- Enrichment of Some Chemicals in Fine Particles
- Mass Emission Transients from Soot Blowing

# Particle Formation - Large Particles



Formation of Coke and Ash Particulate

# Particle Formation - Fine Particles

- Formation mechanism
- 0.5 micron “limit”
- Species & particle surface area

# Pulverized Coal Particulate

- Size
- Process
- Combustion time vs residence time



# Example 5-3.

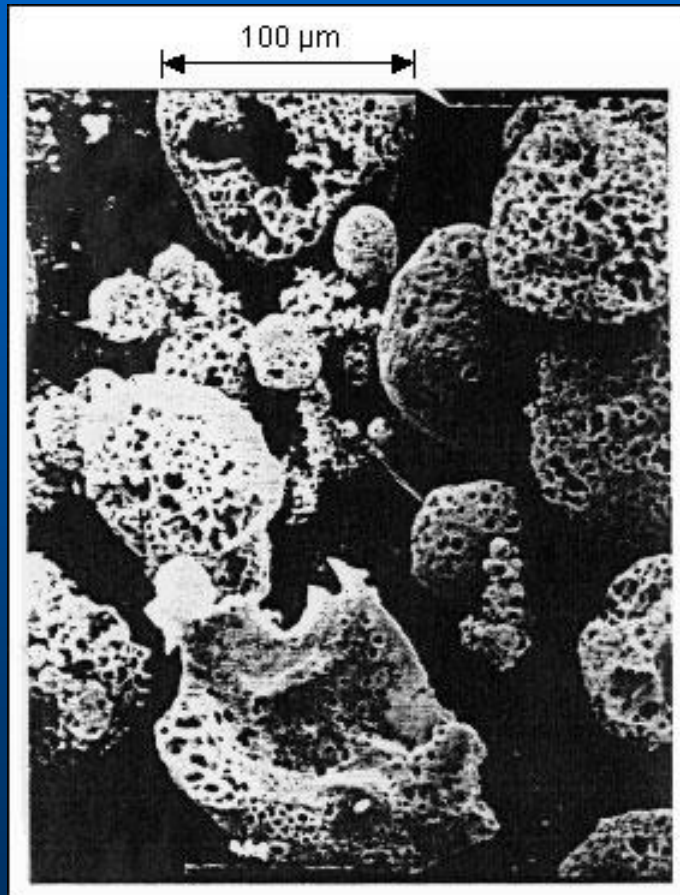
- Determine potential emissions for a PC furnace with coal properties are 9% ash and 12,500 BTU/lb. Assume 10% ash retention and no control.
- Solution:

$$0.09 \left( \frac{\text{lb ash}}{\text{lb coal}} \right) \div 0.0125 \left( \frac{\text{mmBTU}}{\text{lb coal}} \right) \times 90\% = 6.48 \left( \frac{\text{lb particulate}}{\text{mmBTU}} \right)$$

# #6 Oil Emissions

- Particulate from
  - Ash
  - Sulfate
- Carbon
  - Coke
  - Soot (smoke)

# Particulate from No. 6 Oil



# Black Smoke

- Formation
- Combustion conditions required
  - Fuel rich area
  - Flame quenching
- Natural gas flames

# Sulfuric Acid and Sulfate Particulate

- Acid or particulate or measurement method
- Coal-fired sulfate
- Oil-fired sulfate
- Formation factors
  - Fuel sulfur content
  - Vanadium
  - Excess air
  - Boiler ash deposits & temperatures

# Example 5-4

A boiler fires #6 oil containing 1.4% sulfur and HHV = 18,500 BTU/lb. How much particulate is formed if 2% of the sulfur is oxidized to sulfate?

Solution:

$$0.014 \left( \frac{\text{lb S}}{\text{lb oil}} \right) \div 0.0185 \left( \frac{\text{mmBTU}}{\text{lb oil}} \right) \times \frac{96}{32} \left( \frac{\text{lb SO}_4}{\text{lb S}} \right) \times 2\% = 0.045 \left( \frac{\text{lb particulate}}{\text{mmBTU}} \right)$$

# Enrichment of Some Chemicals in Fine Particles

**Table 5-2. Some Elements Enriched in Fine Coal Fly Ash**

Antimony	Gallium	Sodium
Arsenic	Lead	Thallium
Beryllium	Molybdenum	Uranium
Cadmium	Nickel	Vanadium
Chromium	Potassium	Zinc
Copper	Selenium	

# Mass Emission Transients from Soot Blowing

- Most emissions are emitted directly
- Ash accumulation
- Soot blowers
  - Purpose
  - Typical operation
  - Air pollution impacts



# Metals (outline)

- Volatility of Metals and Compounds
  - Determines fine or coarse particle size
  - Affects health risk
  
- Mercury

# Volatility of Metals and Compounds

- Examples – Table 5-3
- Vapor species vs vapor pressure
- Chloride compounds

# Mercury

- Combustion emissions – vapor phase
- Emission sources
  - Municipal waste
  - Coal fired utilities
- Chemical forms
- Environmental fate

# Example 5-5. Mercury emissions

Determine daily mercury emissions for an 800-megawatt power plant. Plant heat rate is 9900 BTU/kw-hr with a 60% utilization factor. It burns coal with 0.13 ppm mercury and HHV = 11,900 BTU/lb.

Solution:

(a) Determine emissions rate

$$0.13 (10^{-6}) \left( \frac{\text{lb Hg}}{\text{lb coal}} \right) \div 0.0119 \left( \frac{\text{mmBTU}}{\text{lb coal}} \right) = 10.9 (10^{-6}) \left( \frac{\text{lb Hg}}{\text{mmBTU}} \right)$$

# Example 5-5 (cont'd)

(b) Determine daily energy use:

$$800,000(\text{kw}) \times 9900 \left( \frac{\text{BTU}}{\text{kw} - \text{hr}} \right) \times 60\% \times 24 \left( \frac{\text{hr}}{\text{day}} \right) = 114,048 \left( \frac{\text{mmBTU}}{\text{day}} \right)$$

(c) Multiply energy use x emissions rate:

$$10.9 (10^{-6}) \times 114,048 = 1.24 \text{ lb/day Hg emissions}$$

# Nitrogen Oxides (outline)

- Overview of  $\text{NO}_x$
- Thermal  $\text{NO}_x$  Formation
- $\text{NO}_x$  Formation from Fuel Nitrogen
- Premixed and Diffusion Combustion
- $\text{NO}_x$  from Typical Combustion Systems
- Control covered in Chapter 6

# Overview of $\text{NO}_x$

- $\text{NO}_x = \text{NO}_2 + \text{NO}$
- $\text{NO}_2$  used for weight
- Ambient concentrations
- Ozone formation
- Other oxides
- All combustion makes  $\text{NO}_x$ :  $\text{N}_2 + \text{O}_2 \leftrightarrow 2\text{NO}$

# Control Approaches

- Two approaches
  - Combustion strategies
  - Back-end controls



# Formation Mechanisms

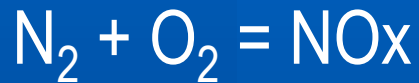
- Thermal NO<sub>x</sub>
- Fuel NO<sub>x</sub>
- Prompt NO<sub>x</sub>

# Typical Emission Rates

**Table 5-4. AP-42 data for Uncontrolled NO<sub>x</sub> Emissions**

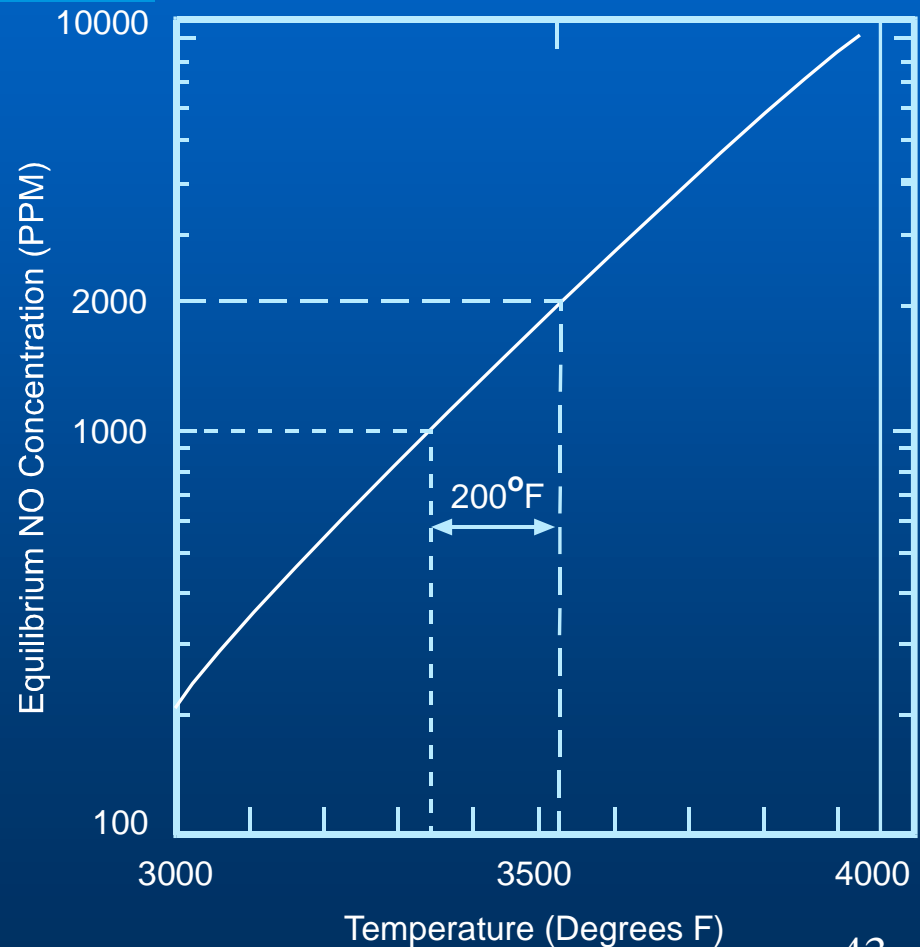
<i>Combustion Source</i>	<i>AP-42 Units</i>	<i>Heat Input Units</i>
Combustion Turbine	67.8 lb/1000 gal. fuel	0.5 lb/mmBTU
Diesel Engine	500 lb/1000 gal. fuel	3.7 lb/mmBTU
Utility Boiler Firing No. 6 Oil	67.8 lb/1000 gal. fuel	0.46 lb/mmBTU
Commercial Boiler Firing No. 2 Oil	20 lb/1000 gal fuel	0.15 lb/mmBTU
Pulverized Coal Boiler	21 lb/ton coal	0.81 lb/mmBTU
Wood Fireplace	1.8 lb/ton wood	0.15 lb/mmBTU

# Thermal NO<sub>x</sub> Formation



Modeling in real flames is complex

No significant decomposition



# NO<sub>x</sub> Formation

- Fuel impacts on NO<sub>x</sub>
  - Amount formed
  - Control techniques
- Analytical approaches to predicting NO<sub>x</sub>?

# NO<sub>x</sub> Formation from Fuel Nitrogen

- Fuel nitrogen can:
  - react with oxygen to form NO, or
  - react with another N atom to form N<sub>2</sub>
- Affects boilers, not engines

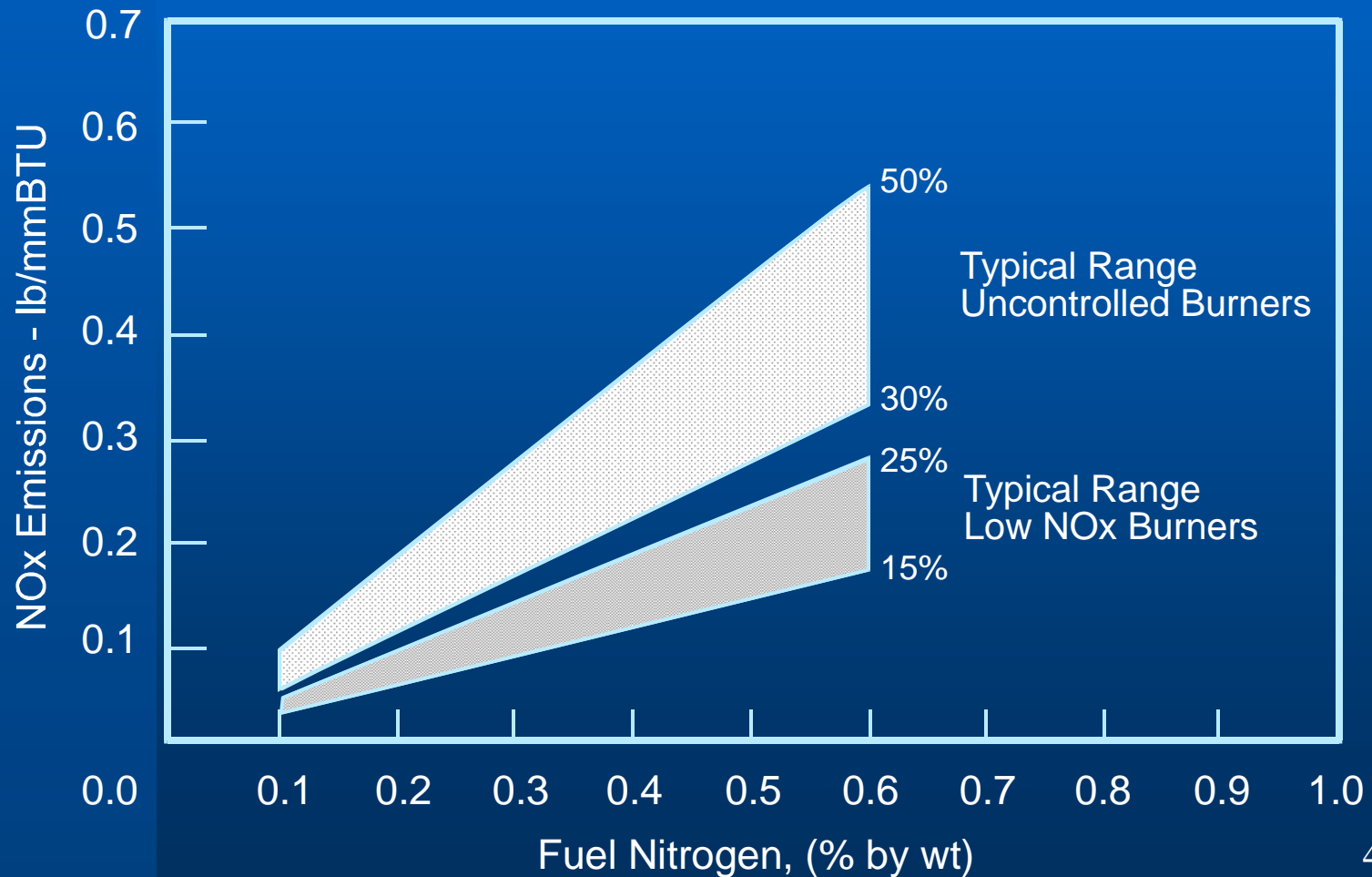
# Example 5-6. Fuel NO<sub>x</sub>

A utility fires coal with 1.3% N and HHV = 13,200 BTU/lb.  
Find the potential NO<sub>x</sub> emissions from fuel N.

Solution:

$$0.013 \left( \frac{\text{lb N}}{\text{lb coal}} \right) \div 0.0132 \left( \frac{\text{mmBTU}}{\text{lb coal}} \right) \times \frac{46}{14} \left( \frac{\text{NO}_2}{\text{N}} \right) = 3.2 \left( \frac{\text{lb NO}_x}{\text{mmBTU}} \right)$$

# NOx Emissions vs. Fuel Nitrogen



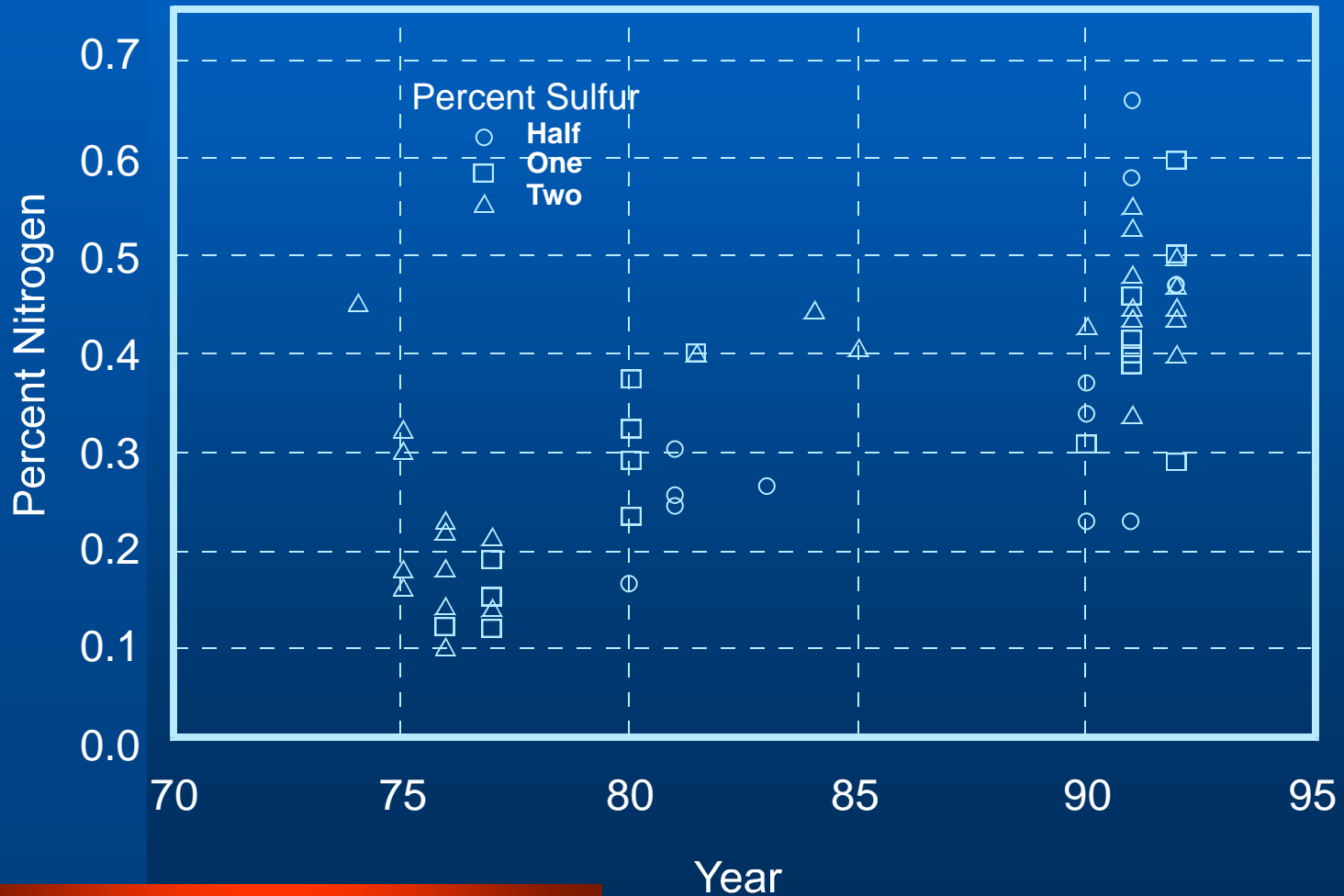
# Typical Fuel N

**Table 5-5. Typical Fuel Nitrogen Content**

<u><i>Fuel</i></u>	<u><i>Nitrogen (% by wt.)</i></u>
Coal	0.5 - 2
Residual Oil	0.3 - 0.6
No. 2 Oil	< 0.1



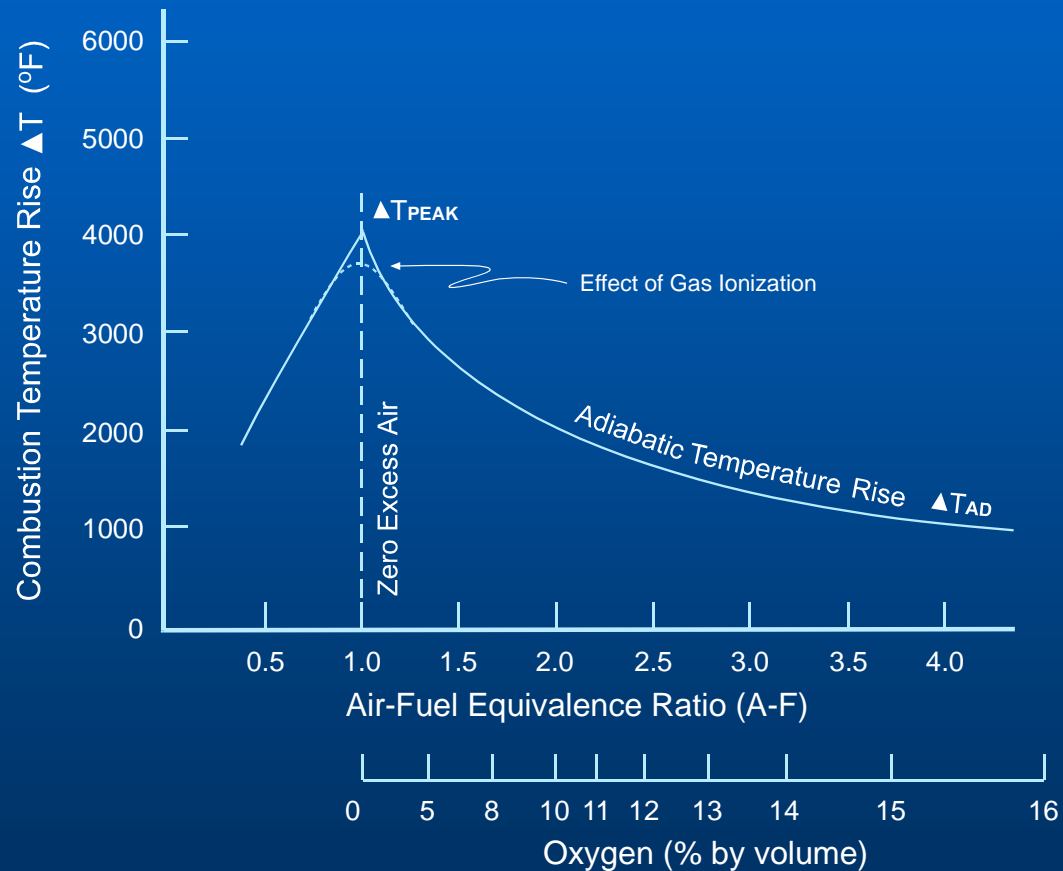
# Residual Oil Nitrogen vs. Time



# Premixed and Diffusion Combustion

- Diffusion
  - Typical of most combustors
- Premixed
  - Gas & gasoline reciprocating engines
  - Some low NO<sub>x</sub> combustors
- Temperatures of premixed & diffusion flames (Fig. 4-5)
- O<sub>2</sub> concentrations

# Premixed and Diffusion Combustion (cont.)



# NO<sub>x</sub> from Typical Combustion Systems (outline)

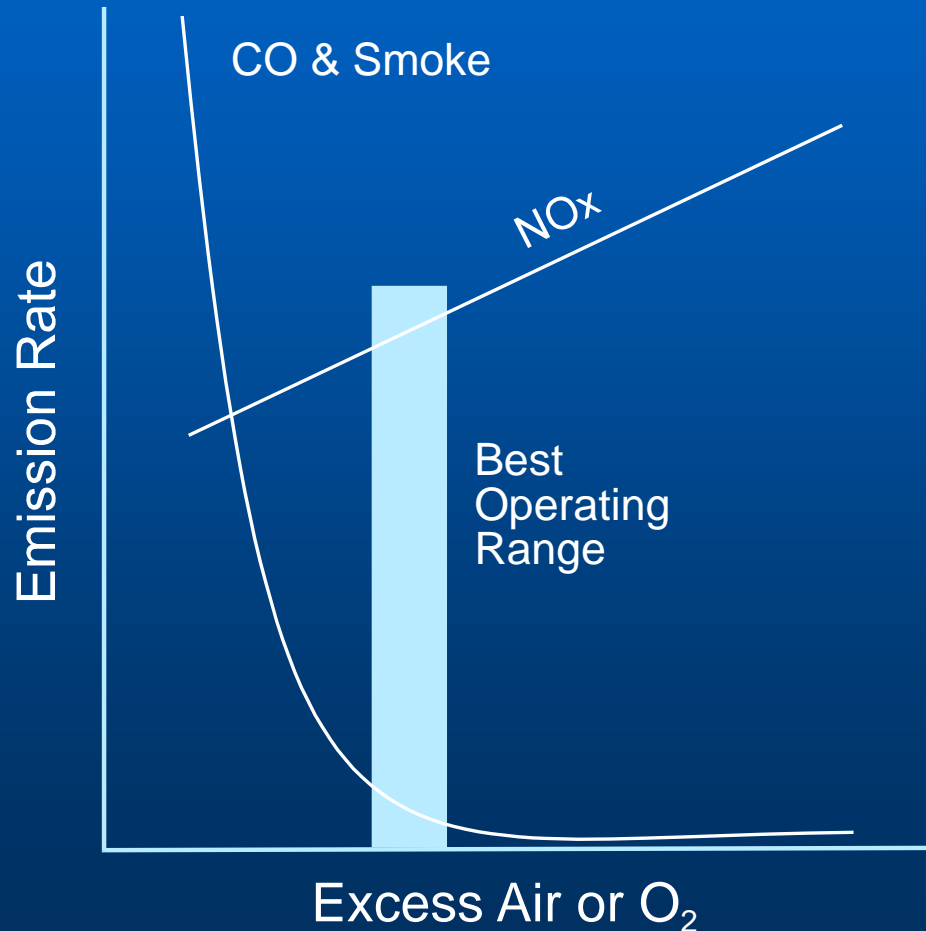
- History of NO<sub>x</sub> control
  - Combustion versus back end
- Combustor categories
  - Boilers and Furnaces
  - Reciprocating Engines
  - Combustion Turbines
- Load range impacts

# NO<sub>x</sub> from Boilers and Furnaces

- Wide range of sizes & fuels
- Temperatures
- Air & fuel flow control
  - Matching air to fuel
  - Trade off of PIC & NO<sub>x</sub> (Fig. 5-9)

# NO<sub>x</sub> from Boilers and Furnaces (cont.)

Typical NO<sub>x</sub> and CO vs. Excess Air



# Fuel Effects on Boiler Emissions

- Three fuel categories:
  - (1) Clean fuels
  - (2) Residual oil, pulverized coal sander dust
  - (3) Solid fuels

# Fuel Effects on Boiler Emissions (cont.)

- Suspension versus grate burning
- Size implications
  - Small boilers =?? Clean fuel
  - Multiple burner implications

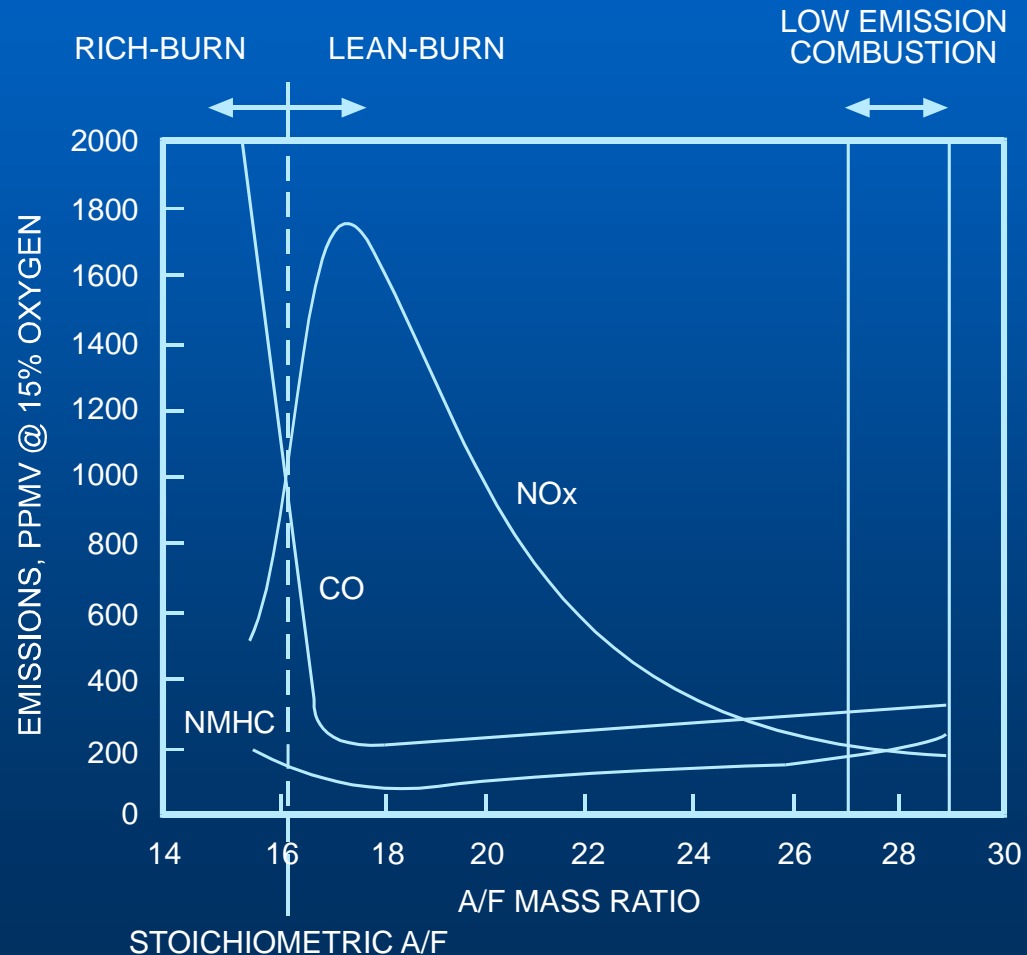


# NO<sub>x</sub> from Reciprocating Engines

- Fuels
- Operating temperature & pressure
- NO<sub>x</sub> emission levels (Fig 5-10)
- Diesel versus gas engines
  - Diffusion vs premix
  - Rich burn & lean burn
- Emission predictability

# NO<sub>x</sub> from Reciprocating Engines (cont.)

Emissions vs.  
Excess Air for Gas  
Fired Engines



# Combustion Turbines

- Overview
  - Aircraft derivative
  - Steady state combustion
  - Traditional versus new “low NOx” combustors
- Fuel flexibility
- NOx emissions
  - Use of water injection
- Predictability
  - Integration of engine & emission controls
  - Ambient conditions

# Smoke, Carbon Monoxide & Organic Compounds (outline)

- Complete Combustion and Fuel-Air Mixing
- Burner Geometry
- Excess Air
- Incinerator Temperatures
- Dioxin-Furan Formation

# Complete Combustion and Fuel-Air Mixing

- PIC
  - Organics (VOC)
  - Smoke (carbon) & CO
  - Startup & transient operation
- CO
  - Surrogate for organics
  - Typical levels

# Elements of Complete Combustion

- Effective fuel air mixing
- Sufficient O<sub>2</sub>
- No quenching

# 3 T's of Combustion

- Time
- Temperature
- Turbulence

# Burner Geometry

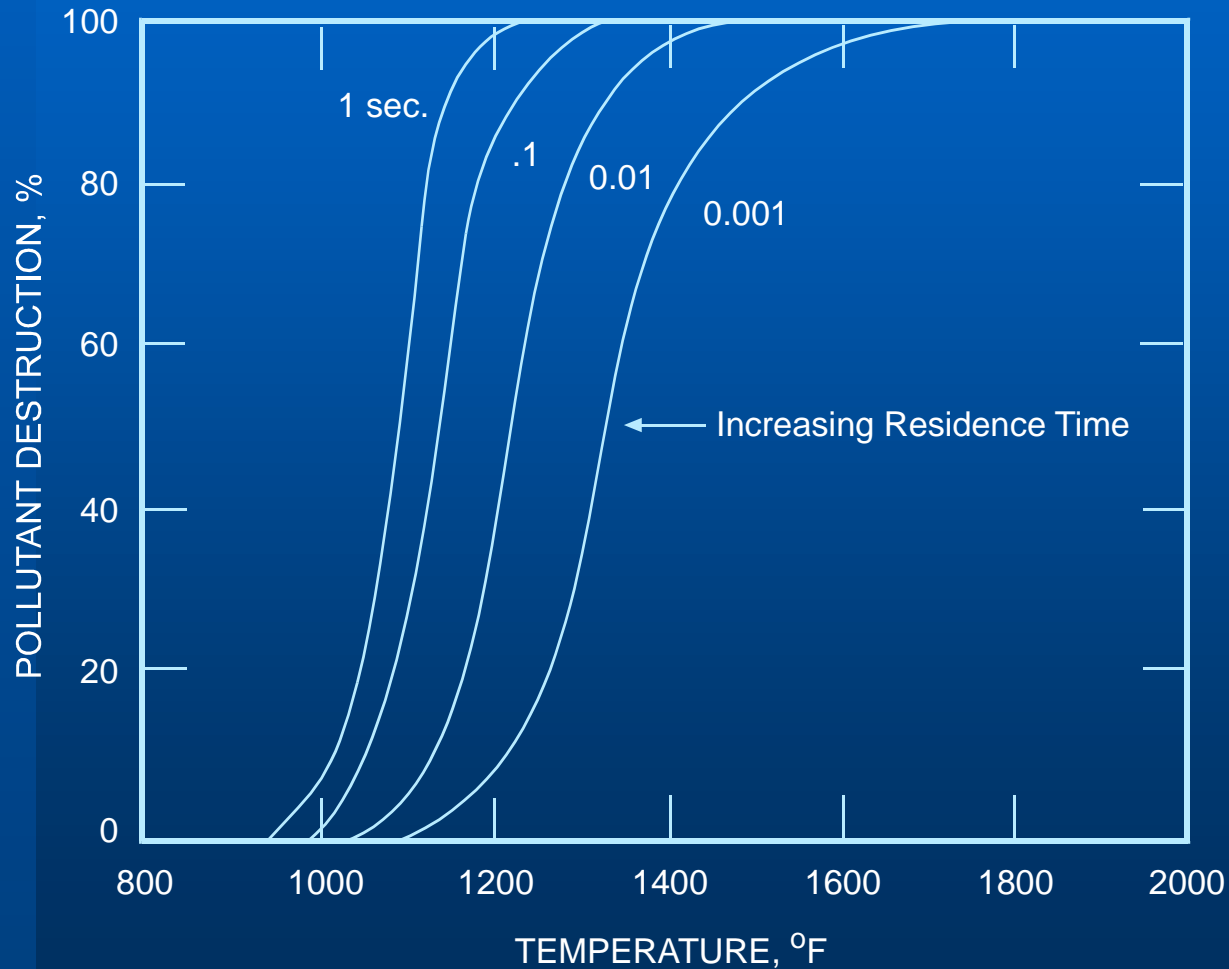
- Objective: complete, fast fuel-air mixing
- Geometry (design) governs mixing
  - Air flow pattern
  - Fuel injection pattern
- Good mixing → low PIC emissions
- Low NO<sub>x</sub> combustion is different



# Excess Air (review)

- A basic requirement
- Burner performance characterized by LEA
- Minimum (& maximum) excess air levels
- Operating for no smoke versus low NO<sub>x</sub>

# Incinerator Temperatures



# Solid Waste Incinerators

- Basic design is important
  - Nonuniform combustion is a given
- High temperatures typically necessary
- Good excess air control

# Dioxin-Furan Formation

- PCDD and PCDF
  - Stable & persistent
  - Combustion generated
- Toxicity
  - Very low levels are of concern
- PIC formation
  - Mostly from Cl aromatics, but . . .
  - Some organic fragments required
- Sources
  - Transformer fires, bad incinerators, forest fires
- Elimination

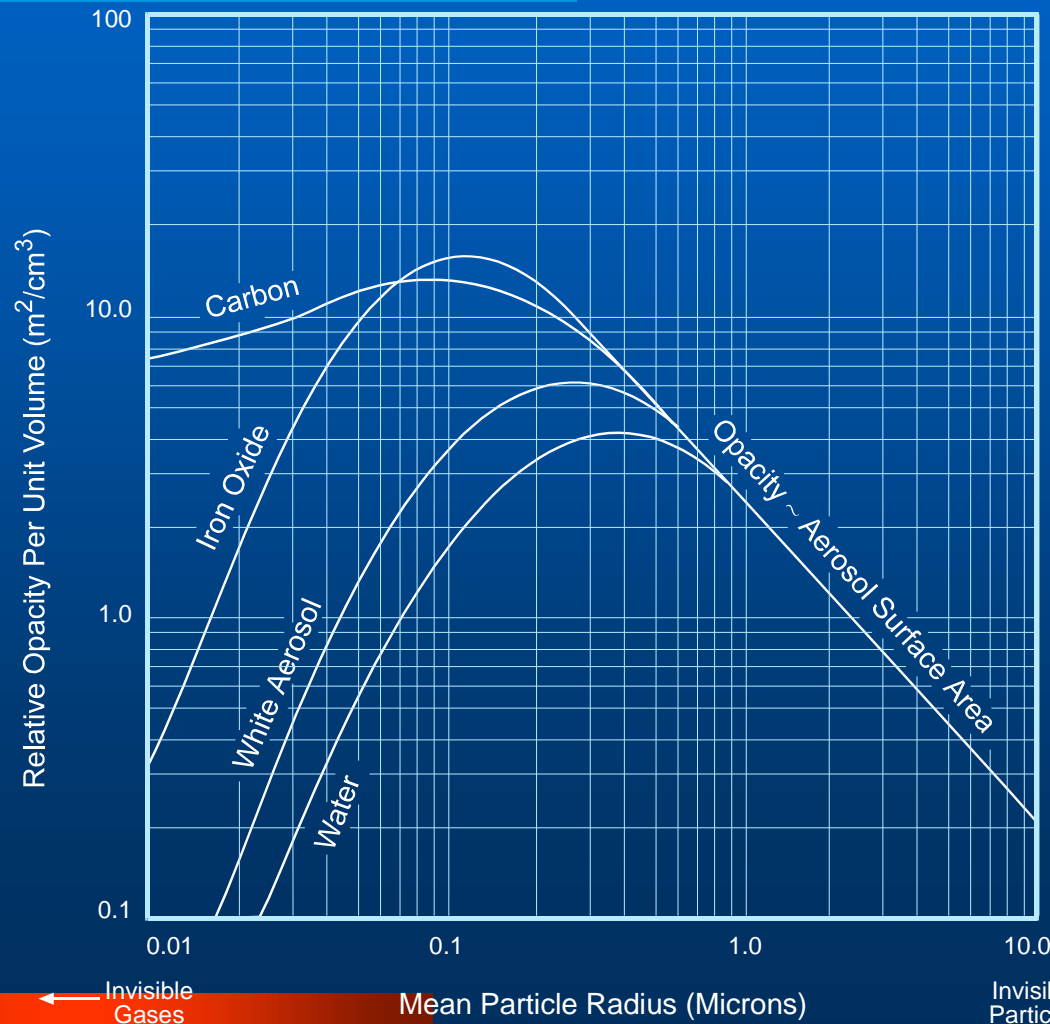
# Dioxin-Furan Formation (cont.)

- Back end formation
  - 500°F
  - Cl<sub>2</sub> & organic PIC
- Avoidance

# Opacity

- Regulatory background
- Method 9 versus Method 5
- Opacity vs. Particle Size

# Dust Opacity vs. Particle Size



# Opacity vs. Emission Rate

- Coal fired particulate emissions
- Residual oil-fired particulate
  - Mass emissions
  - Black plumes
  - White, brown, misc. plumes
- Sulfuric acid mist opacity



# Conclusions

- Emission generating mechanisms
- Pollutant quantity – conservation of mass
- Combustion influence on PIC and NOx
- Particulate emissions
  - Large particles
  - Fine particles

# Chapter Summary

- Introduction
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- Metals
- Nitrogen Oxides
- Smoke, Carbon Monoxide & Organic Compounds
- Opacity